

Numerical and Physical Modeling of the Effect of Roughness Height on Cavitation Index in Chute Spillways

Abstract

This Study presents the results of physical and numerical modeling of the effect of roughness height of chute spillways on the cavitation index. A 1:50-scale physical hydraulic model of the chute spillway of Surk Dam was constructed at the hydraulic laboratory of Shahrekord University, Iran. The experiments were conducted for different flow rates and the parameters of pressure, velocity, and flow depth in 26 positions along the chute. Finally, the ANSYS-FLUENT model was calibrated in the chute spillway using the experimental data by assumptions of two-phase Volume of Fluid (VOF) and k- ϵ (RNG) turbulence models.

The cavitation index in different sections of the chute spillway was calculated for different values of bed roughness including the roughness heights of 1, 2, and 2.5 mm. Results showed that the minimum values of the cavitation index were 0.2906, 0.2733, and 0.2471 for the roughness heights of 1, 2 and 2.5 mm, respectively. The statistical significance analysis showed that reducing the roughness height from 2.5 to 1 mm would not change significantly the value of the cavitation index at 95% confidence interval.

Keywords: Physical model, Spillway, Cavitation, ANSYS-FLUENT Software

Introduction

Chutes and ogee spillways are taken into account as the most important structures used in dam construction. These types of structures are at the risk of cavitation due to the high level and velocity of water flow [1]. Cavitation is the formation of vapor cavities in a liquid, which occurs at high-velocity flow, where the water pressure is reduced locally because of irregularities in the flow surface. As the vapor cavities move into a zone of higher pressure, they collapse, producing high-pressure shock waves. If the cavities collapse near a flow boundary, there will be damage to the material at the boundary [2]. Cracks, ramp offsets and

26 surface roughness can increase the potential for cavitation damage. Many high-height Dam
27 spillways are at the risk of damage due to the occurrence of the cavitation phenomenon.
28 Three factors that contribute to the damage on spillway are flow velocity; material strength;
29 and operating time [3]. Inozemtsev (1969) [4] studied the possibility of the occurrence of
30 cavitation, particularly in high-velocity flows at the first part of spillway downstream, which
31 can contribute to severe damages or structural failure. Kells and Smith (1991) [5] proposed a
32 method for preventing or reducing cavitation damage on spillways using spillway aerators
33 and they presented design considerations and criteria for the spillway aerators using physical
34 hydraulic models. Studies also revealed that air entrainment increases with increase in Froude
35 number, ramp height and cavity pressure.

36 Rajasekhar et al. (2014) [6] investigated the impact of existing voids on the spillway surface
37 and proposed strategies to improve the cavitation resilience of the Sagar Dam spillway
38 (India), the groovheight of 124.66m, located in the Krishna River using a numerical
39 modelling approach. Tests were carried out at different flow rates on a 1:80 scale model and
40 results revealed that in addition to the design flow rate, negative pressure exists even at flow
41 rates below it. Based on the negative pressure measurement and cavitation index
42 computation, the study concluded that cavitation leads to the corrosion of spillway surface
43 and proposed aeration and creation of transverse grooves like the best and economic solutions
44 to overcome this phenomenon. A 1:24-scale physical hydraulic model for the feasibility
45 design (corrective action study preferred option) of the service spillway at El Vado Dam was
46 constructed at Reclamation's Hydraulics Laboratory in Denver, Colorado. Cavitation index
47 value at the worst location was 0.36, which was greater than 0.20 value at which damage
48 typically occurs. The study concluded that such a spillway design does not require
49 extraordinary aeration ramps or other features to promote air entrainment; cavitation potential
50 can be mitigated with the use of appropriate construction tolerances [7]. Nazari et al. (2015)

51 [8] optimized dimension of the plunge pool and flip buckets of five different spillways using
52 hydraulic model studies. By analyzing the data, relations for dynamic values of maximum
53 and minimum pressures and their location along the flip bucket were extracted. Moreover,
54 their results showed that the entrance and exit sections of the bucket encounter cavitation
55 hazard.

56 Ozturk and Aydin (2009) [9] used ANSYS-FLUENT model to study aeration in three-
57 dimensional simulation of spillways to prevent cavitation phenomenon. Numerical simulation
58 results were compared with the measurements of the spillway physical model; numerical
59 results were in agreement with the experimental results. Dehdar-behbahani and Parsaie
60 (2016) [10] studied flow pattern in Balaroud Dam spillway's guide wall numerically and
61 showed that the RNG-K- ϵ is the best model producing the cross waves along the chute
62 spillway. Eskanadari Sabzi and Afrous (2015) [11] investigated the cavitation in 12 models of
63 USACE¹ ogee spillway type at different slopes using ANSYS-FLUENT and k- ϵ (RNG)
64 turbulence model. They concluded that reduction of the slope of the spillway led to an
65 increase in cavitation index, thus, the likelihood of cavitation occurring plummeted. By
66 performing 30 tests on a physical model with five different values of roughness height,
67 Kamanbedast et al. (2014) [12] found that the coefficient of cavitation decreases as roughness
68 values increase.

69 Ghodousi and Abedini (2016) [13] have examined the effects of slope reduction, changing
70 the slope and transforming it into two slopes, and the convergence of chute transverse in the
71 Dam using WS77 numerical model. The simulation results implied that cavitation index
72 values would be significantly changed by creating two different slopes in the chute spillway.
73 On the other hand, the chute transverse convergence causes an increase in cavitation index.
74 Teng (2017) [14] used the Volume of Fluid (VOF) model to deviate the spillway discharge

¹ US Army Corps of Engineers

75 coefficient and showed that the VOF model reproduces reasonably the physical model.
76 Naseri et al. (2018) [15] used large eddy simulation and volume of fluid models to simulate
77 the turbulence and free surface, respectively. Results showed that when moving the place of
78 the hydraulic jump at the first 25% length of the stilling basin, pressure fluctuations were on
79 average 42.6% more at downstream of the chute spillway in comparison with bottom outlet.
80 Chakib (2018) [16] applied VOF model to simulate air-water interaction on the free surface
81 flow of stepped spillway and showed that the $k-\epsilon$ turbulence standard model is in agreement
82 with the experimental results.

83 In this study, the cavitation phenomenon in Surk Dam spillway was evaluated using a
84 physical model. Additionally, ANSYS-FLUENT software, which solves the Reynolds-
85 Averaged Navier-Stokes (RANS) equations based on the finite volume method [17], was
86 calibrated using experimental data on the above mentioned spillway physical model. The
87 main aim of this study is to investigate the effect of roughness height on the cavitation
88 number along the chute spillway. Because the reduction of roughness height of the chute bed
89 is one of the most appropriate methods for preventing cavitation, it is essential to evaluate the
90 effect of changing the roughness height on the hydraulic parameters and cavitation number.

91 **Materials and methods**

92 **Introducing the studied Dam**

93 In the current study, the spillway of Surk Dam earthen-type clay-core was investigated. Table
94 1 shows some general characteristics of Surk spillway. The Dam was constructed across the
95 Kiar River near Surk village of Chaharmahal Va Bakhtiari Province, west of Iran, with a
96 height of 39 m and an effective reservoir volume of 25 MCM (million m^3), located at
97 longitude and latitude coordinates of $32^{\circ}03'26''N$ and $51^{\circ}03'00''E$ and altitude of 2100 m
98 above sea level (See Fig. 1) . The purpose of the Dam is the water supply for downstream
99 agricultural lands and flood control. The Dam has a chute-type ogee spillway in which the

100 slope varies across the chute direction with a distance of 73m from downstream of the
 101 spillway crest (See Fig.2). The values for the slope of the chute are 14 degree and 28 degree,
 102 respectively, before and after the changes occur. The variations of slope provide conditions
 103 for flow separation with a potential for cavitation phenomenon to occur. Therefore, the
 104 present research has been carried out as Chaharmahal Va Bakhtiari Regional Water
 105 Company's requisition.



Fig 1. Location and view of Surk Dam body and spillway

106 **Table 1. Surk Dam spillway general characteristics**

Parameter	Value/description
Spillway chute and crest width (m)	20
Design flood flow rate (m ³ /s)	231
Spillway ogee equation	$Y=0.216 X^{1.748}$ *
Spillway upstream facing slope	1:1
Approach depth at upstream face of the Spillway crest (m)	1

*where X = horizontal distance, Y = vertical distance from coordination axis

107 **Cavitation Index**

108 Cavitation indices can be used to evaluate the potential for cavitation damage in a spillway chute. The
 109 cavitation index is defined as follows [18]:

$$\sigma = \frac{P - P_v}{\frac{1}{2}\rho V^2}$$

$$(1)$$

Where, σ is the cavitation index, P is the actual fluid pressure on the given point, P_v is the vapor pressure of water, V is average flow velocity and ρ is density of water (kg/m^3). This equation can be rearranged in free-surface overflow spillway by assuming a vertical arc at the bottom as [18]:

$$\sigma = \frac{\frac{P_a}{\gamma} - \frac{P_v}{\gamma} + \frac{P_0}{\gamma} \pm (h/g \times \frac{V^2}{R})}{\frac{V^2}{2g}} \quad (2)$$

where, $\frac{P_a}{\gamma}$ is equal to the ambient pressure; $\frac{P_v}{\gamma}$ is the liquid vapor pressure which is equal to 0.32m water at 25 °C; $\frac{P_0}{\gamma}$ is the head equivalent to water pressure measured in different points of the structure; $\frac{V^2}{2g}$ is the velocity head (m) measured at each level; $h/g \times \frac{V^2}{R}$ is the arc-induced head difference; h is depth of flow (m); R is the radius of curvature; γ is the unit weight of the fluid (N/m^3) and g is the acceleration due to gravity (m/s^2). Due to the measured actual pressure in physical mode, $p = \frac{P_0}{\gamma} \pm (h/g \times \frac{V^2}{R})$ is no longer needed in the ANSYS-FLUENT software. In contrast, given the arc radius of 5.9 m in spillway crest of physical model, the arc-induced difference in elevation will be equal to $\frac{h v_0^2}{88/57}$, which v_0 is the average velocity at the arc place.

Falvey [18] introduced the ranges of cavitation index values for designing spillway, as illustrated in Table 2.

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Table 2. Cavitation indices to be considered in design [18]

Design considerations	Cavitation index
No need for protection against cavitation	>1.8
Modified by the removal of irregularities	0.25-1.8
Design modification	0.17-0.25
Protected by aeration galleries with built steps	0.12-0.17
No protection is possible, and needs a redesign	<0.12

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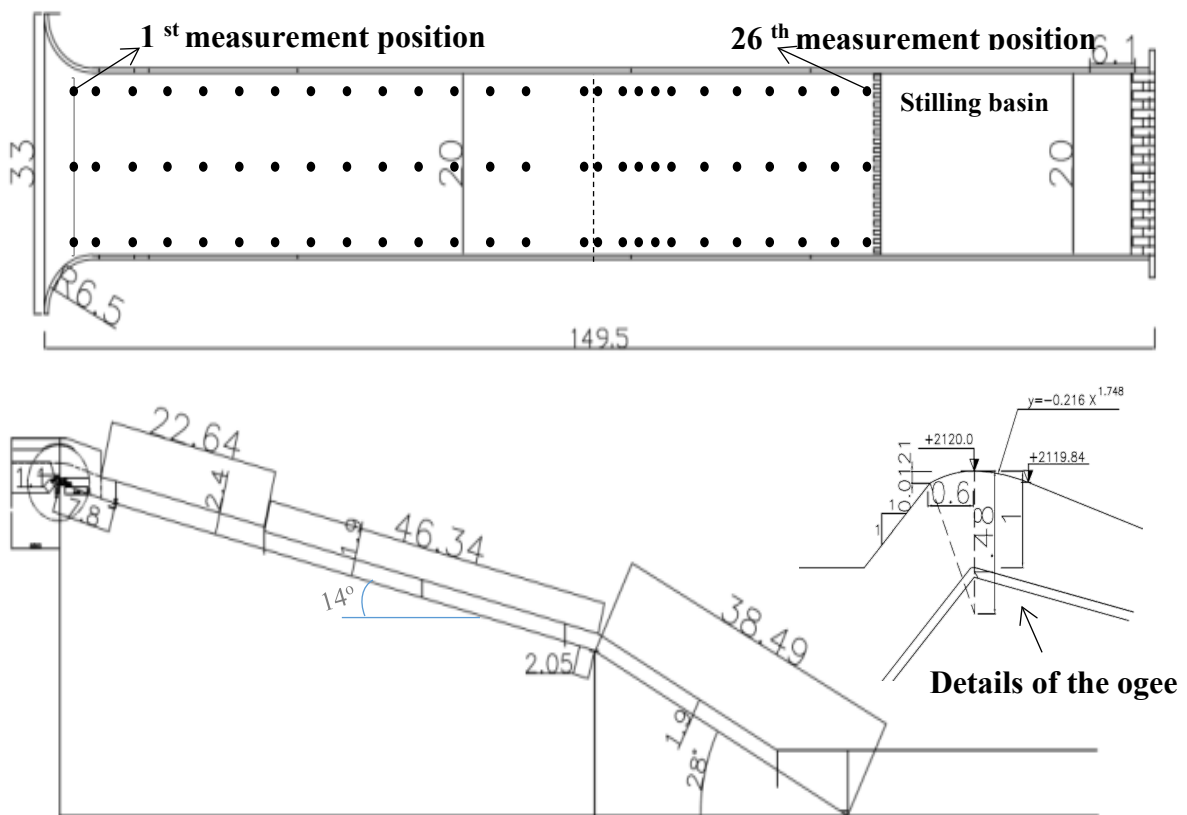
131 Physical Model

132 In addition to the mathematical model, the physical model was used in the current study at
133 **Shahrekord University hydraulic laboratory**. By preparing hydraulic laboratory facilities and
134 providing basic information, the scale of model was specified so that, firstly, **laboratory** space
135 became geometrically and dimensionally adequate; secondly, the existing flow capacity will
136 determine the model dimensions. Based on our survey study and due to the fact that gravity is
137 the dominant force in the free overflow, the physical model was designed based on the
138 dynamic similarity with Froude number with a geometry scale of 1:50. Therefore the physical
139 model was made of Plexiglas with the desired geometric features. **Front and side views of the**
140 **physical model are shown in Figs. 3a and 3b**. The width of the model was 0.4 m and was
141 installed at the end of **the** main flume with 0.6 m width and depth and 20 m length. Pumping
142 system and water cycle in the laboratory **were** capable of supplying up to 70 l/s **flow rate**
143 inside the flume. To ignore viscosity effects, Reynolds number was controlled to be at least
144 10^5 ; additionally, in order to minimize the effect of surface tension and eliminate its adverse
145 effects, Weber number was checked to be always greater than 100 [19].
146 For measuring the **flow rate** a triangle weir set at the end of the system with a notch angle of
147 90 degrees and the following calibrated equation was used;

148 $Q = 1.417H^{2.5}$ (3)

149 Where Q is flow rate (m³/s) and H is the head on the weir (m).

150 In order to measure pressure, piezometers were installed along the chute spillway in 26
 151 positions, as shown in Fig. 2 which the numbers to the top of the figure are the numbers of
 152 the piezometers row. The piezometer tubes were connected to the piezometer tips which were
 153 inserted through holes drilled in the sheet Plexiglas, pasted in place, and finished flush with
 154 the surface. The finishing of piezometers in the models was done meticulously to prevent
 155 measurement errors that would result from improper installation. Sizes of tubing for
 156 connecting piezometers to manometers were selected 2.5 mm inside diameter. For the sake of
 157 convenience, piezometers were placed on board; and in order to achieve high accuracy in
 158 measuring the height of the water column in piezometers, the board was situated at an angle
 159 of 30 degree to the floor in the laboratory [Figs. 3c and 3d].



160

161 Fig. 2. The location of flow parameters measurement in Surk Dam spillway.



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Fig. 3. a. front view of the physical model; b. Side view of the physical model; c. view of piezometers installed; d. the picture of the piezometers board

167 **ANSYS-FLUENT software**

168 FLUENT is capable of solving numerically the Navier-Stokes equations of the turbulent flow,
 169 which have been widely used in computational fluid dynamics (CFD) applications [17]. This
 170 software is one of the most comprehensive computational fluid dynamics software, which
 171 benefits from a finite volume approach to convert the governing equations to the algebraic
 172 ones. For simulating two-dimensional and three-dimensional hydraulic phenomena, different
 173 turbulence models and multiphase problem-solving methods could be taken into account.

174 ANSYS FLUENT's interactive solver set-up, solution, and post-processing make it easy to
 175 pause a calculation, examine results with integrated post-processing, change any setting, and
 176 then continue the calculation within a single application. The integration of ANSYS
 177 FLUENT into ANSYS Workbench provides users with superior bi-directional connections to

178 all major CAD systems, powerful geometry modification and creation with ANSYS
 179 DesignModeler and advanced meshing technologies in ANSYS Meshing. It allows bringing
 180 the easy drag-and-drop transfer of data and results to share between applications (e.g. to use a
 181 fluid flow solution in the definition of a boundary load of a subsequent structural mechanics
 182 simulation). It should be noted that ANSYS FLUENT applies limiting values for pressure,
 183 static temperature, and turbulence quantities. The purpose of these limits is to keep the
 184 absolute pressure or the static temperature from becoming 0, negative, or excessively large
 185 during the calculation, and to keep the turbulence quantities from becoming excessive.

186 **Governing equations**

187 The family of Reynolds-Averaged Navier-Stokes (RANS) models is the most widely used
 188 turbulence modeling approach and offers the most economical approach for computing
 189 complex turbulent industrial flows. In this approach, the Navier Stokes equations split into
 190 mean and fluctuating components. The total velocity u_i is a function of the mean velocity \bar{u}_i
 191 and the fluctuating velocity \acute{u}_i as shown in the following equation [17].

$$192 \quad u_i = \bar{u}_i + \acute{u}_i \quad (4)$$

193 The continuity and momentum equations incorporating these instantaneous flow variables are
 194 given by:

$$195 \quad \frac{\partial}{\partial x_j} (u_i u_j) = -\frac{\partial p}{\partial x_j} + \frac{\partial \tau_{ij}}{\partial x_j} \rho g_i \quad (5)$$

$$196 \quad \frac{\partial u_i}{\partial x_j} = 0 \quad (6)$$

$$197 \quad \tau_{ij} = \left[\rho(\nu + \nu_t) \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \right] - \left[\frac{2}{3} \rho(k + \nu_t) \frac{\partial u_i}{\partial x_i} \delta_{ij} \right] \quad (7)$$

198 Where, u_i is speed agent in x_i direction, u_j is speed agent in x_j direction, p is total pressure, ρ
 199 is fluid density, g is acceleration of gravity, τ_{ij} is stress tensors, ν is kinematic viscosity, ν_t is
 200 turbulence viscosity, k is kinematic energy.

201 **Turbulent models**

202 ANSYS-FLUENT software **is capable of solving** the Reynolds stress terms using a wide
203 range of turbulent models. The accuracy of solving RANS equations depends on the
204 turbulence model to determine the Reynolds stress terms. The k- ϵ and k- ω are two such
205 turbulent models, which provide a good compromise between performance and accuracy
206 [20]. K- ϵ turbulent model is one of the most popular models to simulate turbulent flows,
207 which involves three solutions methods including RNG², standard and realizable. Relying on
208 conducted studies, **RNG-based k- ϵ turbulence model is used in the present study [10 and 11].**
209 **The RNG-based k- ϵ turbulence model is derived from the instantaneous Navier-Stokes**
210 **equations, using a mathematical technique called "renormalization group" (RNG) methods.**
211 **The analytical derivation results in a model with constants different from those in the**
212 **standard k- ϵ model, and additional terms and functions in the transport equations for k and ϵ ,**
213 **which are illustrated as follows [21]:**

$$214 \quad \frac{\partial}{\partial t}(\rho k) + \frac{\partial}{\partial x_i}(\rho k u_i) = \frac{\partial}{\partial x_j} \left(a_k \mu_{eff} \frac{\partial k}{\partial x_j} \right) + G_k + G_b - \rho \epsilon - Y_M + S_k$$

$$215 \quad (8) \quad \frac{\partial}{\partial t}(\rho \epsilon) + \frac{\partial}{\partial x_i}(\rho \epsilon u_i) = \frac{\partial}{\partial x_j} \left(a_\epsilon \mu_{eff} \frac{\partial \epsilon}{\partial x_j} \right) + C_{1\epsilon} \frac{\epsilon}{k} (G_k + G_{3\epsilon} G_b) - C_{2\epsilon} \rho \frac{\epsilon^2}{k} - R_\epsilon +$$

$$216 \quad S_\epsilon \quad (9)$$

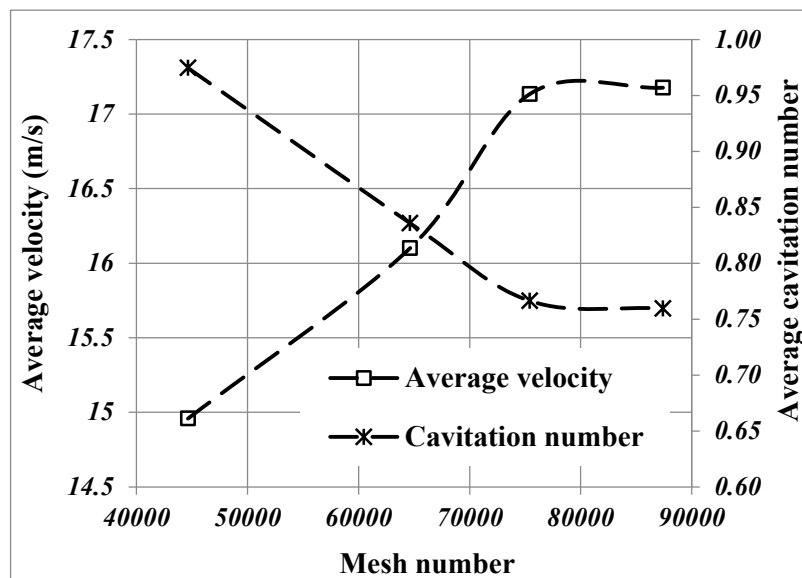
217 Where, **G_k** represents the generation of turbulence kinetic energy due to the mean velocity
218 **gradients, G_b** is the generation of turbulence kinetic energy due to buoyancy, **Y_M** represents
219 **the contribution of the fluctuating dilatation in compressible turbulence to the overall**
220 **dissipation rate, R _{ϵ}** is an additional term in the ϵ equation, the quantities α_k and α_ϵ are the
221 **inverse effective Prandtl numbers for k and ϵ , respectively, S_k and S _{ϵ}** are user-defined source
222 **terms, C_{1 ϵ} , C_{2 ϵ} and C_{3 ϵ}** are constants and μ_{eff} is effective viscosity.

223 **Meshing process and model evaluation**

² Re-Normalisation Group

224 Surk Dam spillway model was meshed with Gambit software. Gambit is a software package
 225 designed to help analysts and designers build and mesh models for computational fluid
 226 dynamics (CFD) and other scientific applications. Gambit receives the user input by means of
 227 its graphical user interface (GUI). The Gambit GUI makes the basic steps of the building,
 228 meshing, and assigning zone types to a model simple and intuitive, yet it is versatile enough
 229 to accommodate a wide range of modeling applications.

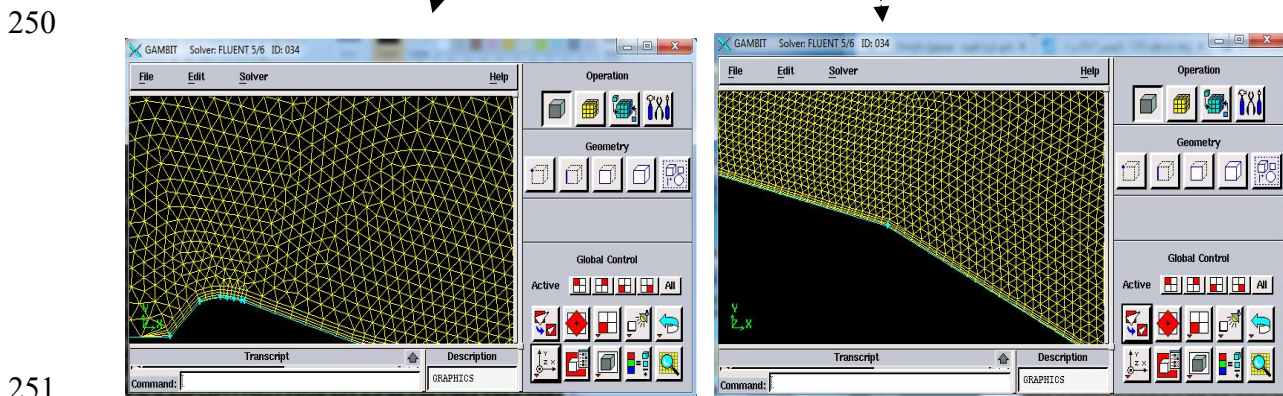
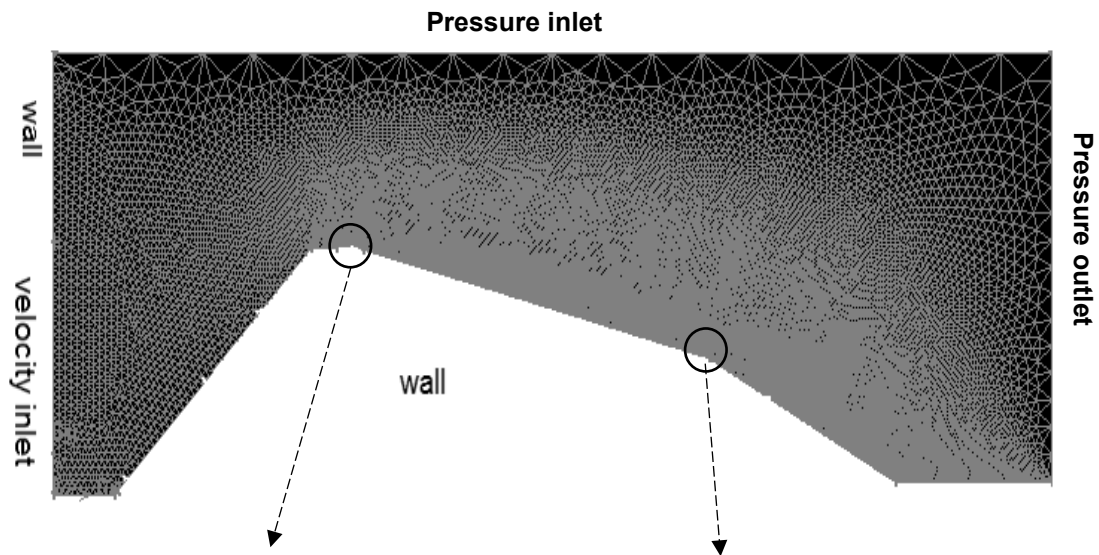
230 In order to reduce the scaling effects in the numerical simulation, the model was designed and
 231 implemented in its true dimensions. In order to accomplish the mesh-independent process as
 232 a part of the model calibration, the model was run with four meshing numbers including
 233 87412, 75432, 64624 and 44631 triangular cells. Comparing the results of the model with
 234 87412 and 75432 cells showed no significant difference (See Fig.4). For all cases, therefore,
 235 the same mesh with 75432 elements was considered in this study.



236
 237 Fig.4. Validation of mesh independency, average velocity and cavitation number versus mesh
 238 number

239 In addition, to obtain a numerical model with the highest level of accuracy, the boundary
 240 layer element was applied in the numerical simulation. Boundary conditions were imposed on
 241 the numerical model with the numerical models and assumed as the following [Fig.5]:

- 242 1. Inlet boundary condition at **the** inlet, the velocity of flow was considered to set up to
- 243 the reservoir water level and above that it was considered as a fixed wall
- 244 2. Outlet boundary condition, the outflow was set as pressure outlet, to have constant
- 245 pressure outflow
- 246 3. Wall condition, the wall was considered to be at the surface concrete of the chute
- 247 spillway
- 248 4. The top of the domain area was assigned as pressure outlet. Moreover, the initial
- 249 condition was imposed taking the velocity at the entrance into account.



252 **Fig. 5. Surk Dam spillway boundary conditions and the mesh network**

253 **Two-phase flow solution**

254 Since the cavitation is a two-phase phenomenon consisting of atmosphere and water, **VOF**

255 model was used for two-phase flow simulation and surface calculations. VOF method is

256 based on the principle that two or more fluids are not combined together. For each phase in
 257 the model, one variable is regarded as that phase volume fraction in the computational cell. In
 258 each control volume, the total volume fractions for all phases are equal to one. The fluid-
 259 volume scheme is assumed to have a point boundary between two phases at which the
 260 numerical value of the volume fraction parameter is 0.5 [22]. There are three possibilities of
 261 fluid volume fraction (a_q) in the cell as,

- 262 A.) $a_q = 0$, cell is devoid of fluid.
- 263 B.) $a_q = 1$, cell is full of fluid.
- 264 C.) $1 > a_q > 0$, cell owns joint surface between two or more fluids.

265 In this study, the simulations were performed with five flow rates, as illustrated in table 3,
 266 and with respect to the measured values of the flow parameters, such as pressure, velocity,
 267 and flow depth, the model was calibrated and validated by changing of the roughness height.
 268 The calibrated value of the roughness height was obtained at 2.5 mm. Finally, the cavitation
 269 index was calculated at all positions which are shown in Fig. 2. If the numerical results were
 270 in a good agreement with the experimental data, the numerical model would be appropriate
 271 for our numerical study.

272 **Table 3. Different flow discharge values used in this study**

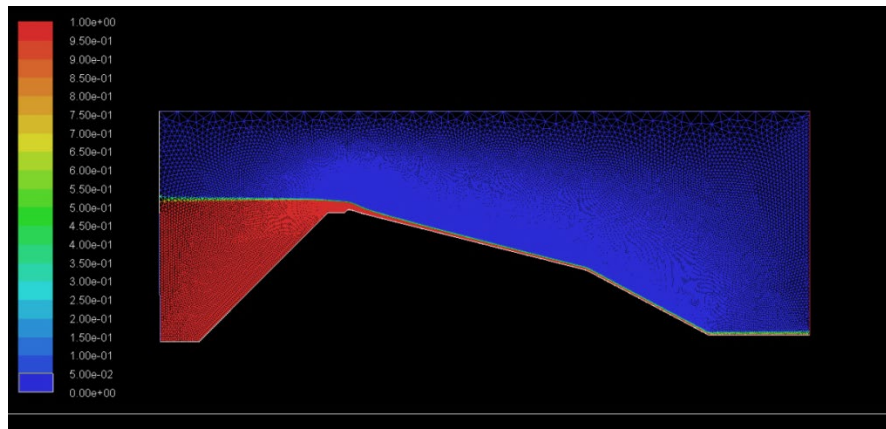
Exp. No.	1*	2	3	4	5
Flow rate in prototype (m³/s)	234	176.73	151.70	110.80	73.41
Flow rate in physical model (l/s)	13.24	10.00	8.58	6.27	4.15

* Design flow rate

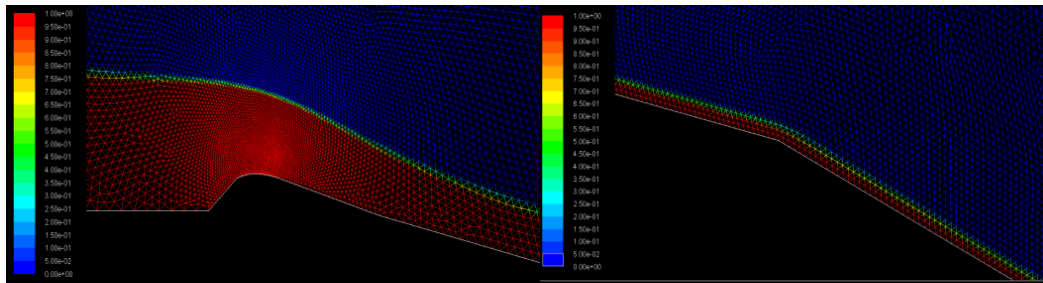
273 Results and discussion

274 ANSYS-FLUENT model was calibrated using experimental data from the physical model.
 275 After model calibration, the simulation of data was performed for model verification at flow
 276 rates lower than the design flow rate, and the results were compared with those achieved from

277 the physical model. Fig. 6 shows a view of the water surface flow through the spillway from
 278 the numerical model.



279



280

281 Fig.6. A view of the water surface flow through the spillway from the numerical model.

282 Results of the simulated model were evaluated by calculating the root-mean-square error
 283 (RMSE) and normalized root mean square error (NRMSE). Table 4 represents a comparison
 284 of different parameters in ANSYS-FLUENT software and physical model. The statistical
 285 parametric equations are defined as:

$$286 \quad RMSE = \sqrt{\frac{\sum(x_l - x_m)^2}{n-1}} \quad (10)$$

$$287 \quad NRMSE = \frac{RMSE}{\bar{x}_l} \times 100$$

288 (11)

289 Where, x_m : the values of numerical model, x_l is lab measured values and n is the number of
 290 data and \bar{x}_l is the mean value of the lab measurements.

291 Also the average values of Reynolds number and Froude number obtained from the physical
 292 and numerical models for different flow rates and RMSE and NRMSE values of these
 293 parameters are illustrated in table 5.

294 Table 4. RMSE and NRMSE values associated with water depth, velocity, and pressure
 295 parameters between experimental and numerical models

Exp. No.	Flow rate (m ³ /s)	Depth		Velocity		Pressure	
		RMSE	NRMSE%	RMSE	NRMSE %	RMSE	NRMSE %
1	234	0.058	6.98	0.574	3.38	0.052	5.28
2	176.73	0.057	7.91	0.723	5.117	0.05	5.07
3	151.7	0.062	10.64	0.921	6.66	0.086	8.61
4	110.8	0.056	10.62	0.741	5.623	0.11	11.65
5	73.41	0.043	10.51	0.68	5.89	0.19	19.89

296 Table 5. Statues of Reynolds number and Froude number obtained from physical and numerical
 297 models

Flow rate (m ³ /s)		234	176.73	151.70	110.80	73.41
Reynolds number	Average values (physical model)	12,787,673	9,347,401	7,488,286	6,152,915	4,153,413
	Average value (numerical model)	12,027,173	8,926,200	7,387,561	5,577,645	4,025,209
	RMSE	1,055,240	692,509	510,398	770,613	482,543
	NRMSE (%)	8.3%	7.4%	6.8%	12.5%	11.6%
Froude number	Average values (physical model)	6.54	5.90	6.17	4.19	6.44
	Average value (numerical model)	6.83	6.31	6.75	4.34	6.72
	RMSE	0.42	0.51	0.63	0.23	0.41
	NRMSE (%)	6.5%	8.6%	10.3%	5.5%	6.3%

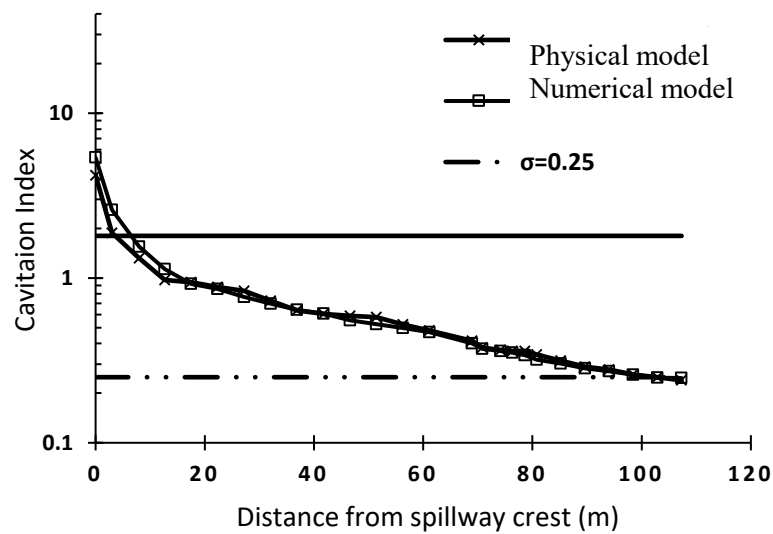
298 Cavitation index in physical and numerical models

299 In order to assess and control the occurrence of cavitation, data such as average velocity and
300 pressure applied on the bottom in different parts of the structure were studied. The necessary
301 data were taken from the two-center axis and the sidewall at different points to calculate the
302 cavitation index. According to equations 1 and 2 and also the values of the parameters
303 obtained from numerical and physical models, the cavitation index was calculated at any
304 section of spillway. In Figs. 7 to 9, the curve of the variations of cavitation index values along
305 the spillway longitudinal axis in numerical and physical models are given for the first, fourth
306 and fifth flow rates. In order to evaluate the accuracy of the numerical model, RMSE,
307 NRMSE and p-value were computed for different flow rates. The results (Table 6) show that
308 there is no significant difference in the cavitation index between experimental and numerical
309 models at 95% confidence interval. That means the accuracy of the numerical model is
310 acceptable at 95% confidence interval [23].

311 The occurrence of cavitation in this study is determined on the observations proposed by
312 Falvey (1990) illustrated in table 2. As indicated by the cavitation rate curves, the measured
313 cavitation index along the Surk Dam spillway has been continuously decreased. According to
314 the Fig. 7 and table 4, it is obvious that when the designed flow rate passes over the spillway,
315 no cavitation protection is needed for up to 3 m in the downstream of the spillway crest. On
316 the contrary, at a distance of 3 m from the spillway crest, cavitation index reaches 1.8 and
317 from this section, the value of the index decrease due to increasing flow velocity. This trend
318 continues to a distance of 103 m from the crest. Based on Falvey's [18] recommendation, the
319 flow range above the Surk Dam spillway should be modified by correcting irregularities and
320 roughness of the concrete surface and any further decline should be prevented.

321 The cavitation index was computed and observed to be less than the critical value ($\sigma = 0.25$)
322 at a flow rate equal to design flow discharge and between 25 and 26 measuring piezometers
323 i.e., at a distance of 103 m from the end of the chute. The lowest cavitation index at 107.3 m

324 from the crest was computed to be 0.249 and 0.237 for the physical model (in the central
 325 axis) and numerical model, respectively. The calculated index in this part of the chute ranges
 326 from 0.17 to 0.25. According to the Falvey's recommendations [18], modifications should be
 327 carried out when a flow rate greater than the designed flow that passes over the spillway to
 328 increase the cavitation index in the Surk Dam spillway. Figs. 8 and 9 demonstrate cavitation
 329 index variations of the fourth (mean) and fifth (least) flow rates. As shown in the figures,
 330 increasing the flow rate reduces cavitation index values so that the index value for the
 331 maximum flow rate to be passed from the critical value at the end part of the chute spillway.
 332 Additionally, at flow rates lower than the design flow rate, cavitation index in the chute
 333 spillway was between 0.25-1.8, which indicates modification requirements by the removal of
 334 irregularities of the chute surface concrete are needed. In this regards, the results from both
 335 numerical and physical models agree.

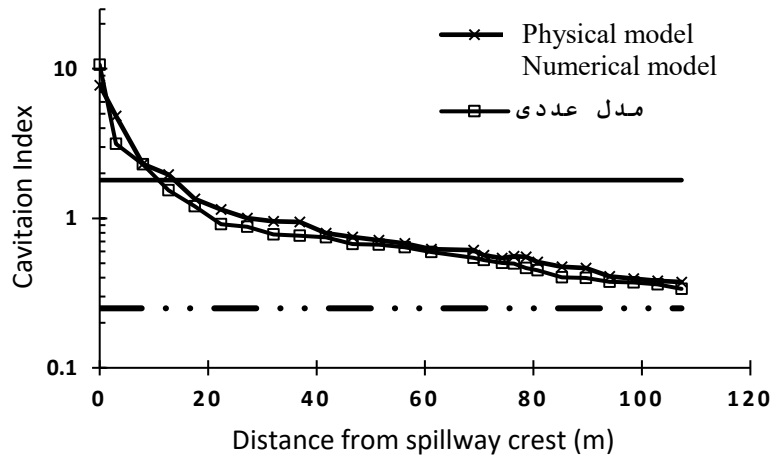


336

337 **Fig. 7. Variations of cavitation index along the spillway in numerical and physical**

338

models at maximum flow rate

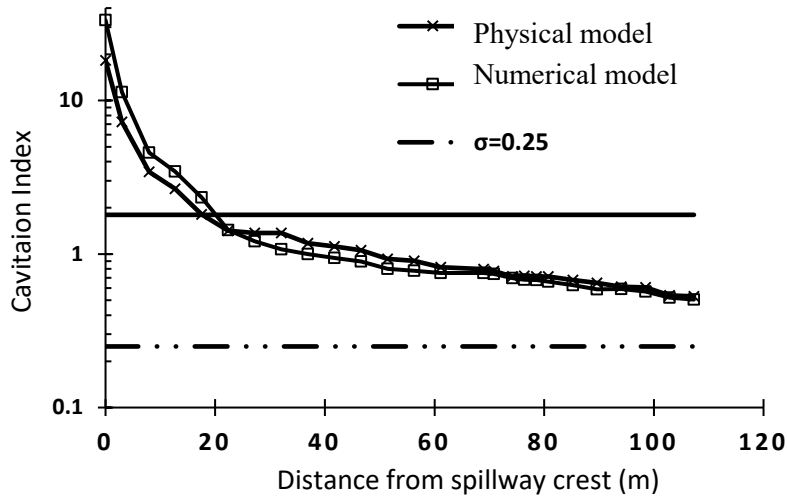


339

340 **Fig. 8. Variations of cavitation index along the spillway in numerical and physical**

341

models for $Q = 110.8 \text{ m}^3/\text{s}$



342

343 **Fig. 9. Variations of cavitation index along the central axis of the chute spillway for $Q =$**
 344 **$73.41 \text{ m}^3/\text{s}$**

345

346

347 **Table 6. RMSE, NRMSE and p-values associated with cavitation index parameters between**

348

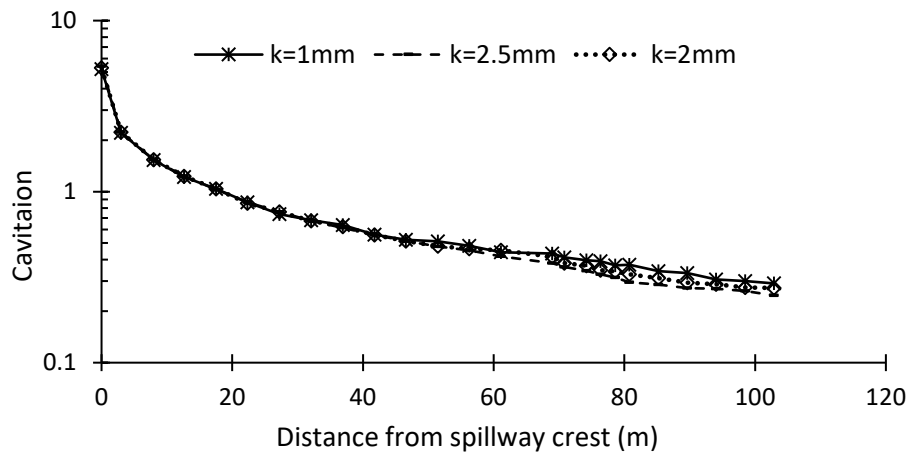
experimental and numerical models

Flow rate (m^3/s)	234	176.73	151.7	110.8	73.41
RMSE	0.081	0.106	0.081	0.165	0.331
NRMSE	9.81%	11.55%	8.55%	15.74%	17.75%
P-Value	0.262	0.430	0.225	0.069	0.375

349 Cavitation index for different roughness heights

350 In light of the results from the current study and Falvey's [18] recommendations,
351 modification the flow by removing unevenness and reducing roughness height is required.
352 Hence, in order to clarify the influence of modifying the chute surface on the variation of the
353 values of the cavitation index, ANSYS-FLUENT numerical model was calibrated for the
354 roughness in the base case. This will help us to choose an optimal roughness for modifying
355 the spillway surface. In addition to the base roughness height ($k_s=2.5$ mm), the model was run
356 for values of roughness height between 1 mm and 2 mm under fixed hydraulic circumstances
357 for the designed flow rate in which the cavitation index was less than the critical value, and
358 then cavitation index was calculated.

359 Fig. 10 illustrates the variations in values of the cavitation index versus distance for different
360 values of roughness height. Fig. 10 shows that the minimum values of the cavitation index
361 are 0.2906, 0.2733, and 0.2471 for the roughness heights 1, 2 and 2.5 mm, respectively. This
362 shows reducing roughness height increases the values of cavitation index, so that the values
363 get away from the critical value stated by Falvey [18]. On the other hand, this decrease
364 maintains the chute of spillway safer against cavitation occurrence compared to the
365 benchmark state. In order to determine the significant level of the effect of the roughness
366 height on the value of the cavitation index, the statistical significance of t-test was done [23].
367 The results of this analysis, as illustrated in table 7, show that based on the p-value
368 (probability), there is no significant difference of the cavitation index between the cases of
369 roughness heights of 2.5 and 2 mm at 95% confidence interval and the same result has been
370 obtained for the cases of roughness heights of 2.5 and 1 mm. These results show that the
371 method of "modified by the removal of irregularities" (See table 2), which causes the
372 roughness height of the chute spillway to be reduced, would not change significantly the
373 value of the cavitation index.



374

375 **Fig. 10.** Variations of cavitation index along spillway for different roughness heights in
 376 numerical model for design flow rate

377

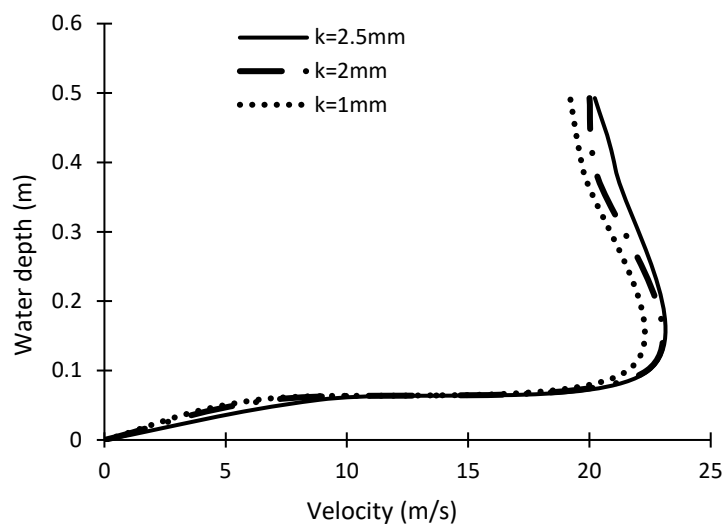
Table 7. The results of statistical significance analysis (t-test)

t-test number	The first t-test		The second t-test	
variable	Variable 1	Variable 2	Variable 1	Variable 2
Ks (mm)	2.5	2	2.5	1
Mean value of σ	0.812932	0.806234	0.812932	0.824065
Variance	1.080619	1.077335	1.080619	1.035429
Observations	26	26	26	26
Pearson Correlation	0.999969		0.999903	
Hypothesized Mean Difference	0		0	
Degree of freedom	25		25	
t Stat	3.992312		-2.12295	
P-value(T<=t) one-tail	0.000269		0.022134	
t Critical one-tail	1.710882		1.710882	
P--value (T<=t) two-tail	0.000537		0.044267	
t Critical two-tail	2.063899		2.063899	

378 The results from numerical modeling also show that the reduction on the roughness height
 379 decreased the mean velocity. Although reducing the roughness height causes an increase in
 380 the flow velocity but any decrease in the roughness height reduces the intensity of flow

381 turbulence. As such, the reduction of flow turbulence causes an increase in the viscosity
382 impact, and flow streamlines will be much more regular compared to the state with higher
383 turbulence. Additionally, the average flow velocity in the boundary layer is reduced [Fig.11].

384 To verify the abovementioned point of view, the velocity profiles along with flow depth were
385 studied. The results show that reducing the roughness height had an impact on the velocity
386 gradient. Fig. 11 shows velocity variations versus the depth values within a distance of 90 m
387 from the crest. As shown in Fig. 11, reduction of roughness height influenced the velocity
388 gradient, leading to the reduction of the average velocity. This reduction in turn results in an
389 increase in the cavitation index at the chute downstream.



390
391 Fig. 11. The variations of velocity distribution by depth for different values of bed roughness
392 heights

393 Conclusions

394 Considering the measured and simulated pressure and velocity, results of flows' cavitation
395 coefficient (cavitation index) revealed that the coefficient of cavitation descends over the
396 chute at any flow rate. The minimum value of the cavitation index was calculated to be 0.242
397 for a flow rate of 234 m³/s at a point located at a distance of 107.2 m from spillway crest.
398 Considering the calculated cavitation coefficient in the flow rates close to the designed flow

399 rate, the possibility for the reduction of the cavitation index and the occurrence of cavitation
400 exists if the surface roughness and design are not modified. The calculation of cavitation
401 index in flow rates less than design flow rate (the second to fifth flow rates) showed that the
402 modification of flow and irregularities existing on the Surk Dam spillway surface is
403 necessary to prevent the cavitation index reduction. Moreover, the effect of changing
404 roughness on the reduction of the cavitation index for the spillway was numerically simulated
405 in ANSYS-FLUENT software. Results showed that reduction of roughness height influenced
406 the value of cavitation index and the velocity gradient, leading to the reduction of the average
407 velocity. Results showed that the minimum values of cavitation index were 0.2906, 0.2733,
408 and 0.2471 for the roughness heights of 1, 2 and 2.5 mm, respectively. Although these results
409 indicate reducing the roughness height increases the values of the cavitation index, so that the
410 values get away from the critical value stated in previous studies but the statistical
411 significance analysis showed that reducing of the roughness height from 2.5 to 1 mm would
412 not change significantly the value of the cavitation index at 95% confidence interval.

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