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1 **Metal organic Framework Enhanced SPEEK/SPSF**
2 **Heterogeneous Membrane for Ion Transport and Energy**
3 **Conversion**

4
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1 ABSTRACT

2 Bioinspired nanofluidic devices have drawn increasing global interest due to their giant
3 applicable potential in a wide range of fields. By mimicking biological prototype, it is
4 expected to achieve high energy conversion efficiency and tunable ion transport.
5 However, the low osmotic conversion efficiency, weak ion transport capability and poor
6 mechanical performance limit practical application. We designed a class of
7 heterogeneous membrane consisting of a support layer and a thin top layer to meet
8 fundamental requirements. To achieve higher power generation, we incorporated metal
9 organic framework (MOF) nanosheets (dispersed phase) into polymer matrix
10 (continuous phase) to afford a mixed matrix top layer. This unique structure addressed
11 the geometric restriction associated with the polymeric specie due to their limited pore
12 accessibility. As a result, the presented membranes produced high power density of *ca.*
13 7 W m^{-2} and a high energy conversion efficiency of *ca.* 40% under a salinity gradient
14 of 50 (0.5 M|0.01 M, NaCl). This work thus offers an insight into a new methodology
15 in the development of a novel membrane technology for highly efficient energy
16 conversion.

17 **KEYWORDS:** energy conversion, salinity gradient energy, mixed matrix membrane,
18 metal organic framework

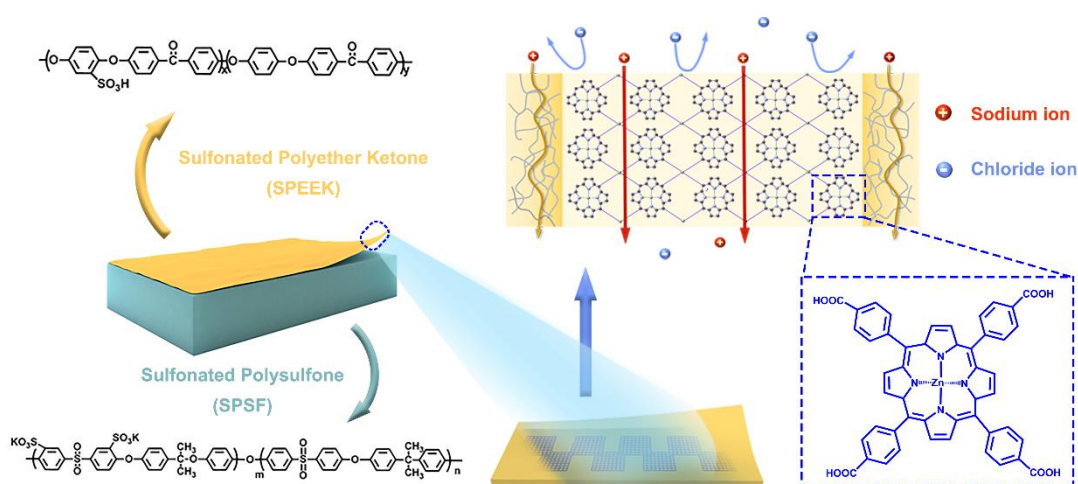
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20 **1. Introduction**

21 Nature provides a unique perspective on power generation because organisms have
22 efficient energy conversion and storage systems *via* ion transport.[1, 2] As ubiquitous
23 phenomena in biology, it lays a solid foundation for complex physiological activity.[3]
24 Typically, directional ion transport could generate more than 100 V electricity through

1 concentration gradient of electrolyte for eel.[4] The electricity directly generates from
2 the Gibbs free energy of mixing through highly concentrated seawater and fresh through
3 ion selective channel,[5, 6] which allows the counter ions to pass through the membrane
4 preferentially, while compelling the common ions as much as possible. The migration
5 of surplus ions thus results in a voltage difference between the two ends of channels. In
6 addition, the ion channel could regulate ion fluxes, ion species and flow directions,
7 which are so-called ion gating, ion selectivity and ion rectification, respectively.
8 Bioinspired nanochannel membranes have been proposed to mimic such biological
9 functions.[7, 8] However, an immediate challenge to achieve high energy conversion
10 and fast ion transport are the low efficiency and poor long-term stability. The polymeric
11 membrane has been reported of harvesting electricity from salinity gradient energy
12 (SGE), but it is limited by low power density and complex preparation processes.[9, 10]
13 Recently, a class of membrane materials, namely heterogeneous composite membrane
14 (consisting of a support layer and a thin top layer), has shown great potential to
15 overcome aforementioned obstacles.[11] The asymmetric structure was recognized as
16 an important factor to improve the ion transport feature **for energy conversion,**
17 **separation and water desalination**[12]. Besides, polymer composite membranes
18 displayed good flexibility and compatibility compared to porous rigid counterparts,
19 such as porous anodic aluminum oxide (AAO), mesoporous carbons and silica
20 membranes. Combining their low-cost effectiveness and easy fabrication nature,
21 heterogeneous membranes have been considered one of the most promising membrane
22 materials. However, one immediate drawback is the geometric restriction, leading to a
23 significant reduction in membrane performance,[13] including channel tortuosity,
24 narrow transport path and wide size distribution. Taking recent advance of mixed matrix
25 membrane in the development of metal organic framework (MOF) nanosheets, we

1 expected to mitigate the geometric restriction and hence further improved the
 2 membrane performance in the process of SGE conversion.
 3 Here, we reported a new approach to prepare a heterogeneous membrane system by
 4 incorporating metal organic framework (MOF) nanosheets as porous fillers into
 5 sulfonated polyether ketone (SPEEK) polymer matrix, which was subsequently coated
 6 onto a sulfonated polysulfone (SPSF)-based substrate (**Scheme 1**). The presented
 7 SPEEK-MOF/SPSF membrane displayed exceptional mechanical stability, tunable ion
 8 flux and enhanced energy conversion capability. The incorporation of ultrathin two-
 9 dimension (2D) MOFs can increase the ion flow rate in a confinement region within
 10 the top layer. In addition, the hierarchical porous structure of the MOF nanosheets will
 11 offer a multidimensional pathway along horizontal direction and voids between
 12 inorganic-organic interface, which can significantly reduce the geometric restriction
 13 effect of the composite configuration. In addition, the output power was further
 14 improved by negative temperature gradient (opposite with salinity gradient) at both
 15 sides of membrane. This study thus opens up a new avenue for the development of
 16 membrane-based technologies for SGE applications.



17
 18 **Scheme 1.** Composite membrane and its chemical composition. The top layer was SPEEK
 19 membrane embed with ZnTCPP MOF and the substrate was SPSF. The addition of 2D nanosheets

1 could shorten ion transport path.

2 **2. Experimental Section**

3 **2.1 Materials**

4 SPEEK and SPSF were purchased from Tianjin Yanjin Technology Co., Ltd. The
5 sulfonation degree was 30%, calculated by ion exchange capacity (IEC) for SPSF. The
6 SPEEK was obtained through concentrated sulfuric acid for 3.5 hours, which
7 sulfonation degree was 85% estimated by NMR (Figure S1)[14]. ZnTCPP nanosheets
8 were synthesized by the solvothermal method. $\text{Zn}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ and polyvinyl
9 pyrrolidone (PVP) were dissolved into the binary solution of DMF and ethanol. Then
10 TCPP was dissolved into binary solution of DMF and ethanol and added to the previous
11 solution dropwise. The solution was transferred into a stainless-steel autoclave at 80°C
12 for 20 h under autogenous pressure. The resultant ZnTCPP nanosheets were washed
13 with ethanol for multiple times and collected by centrifuging (7800 rpm). A
14 heterogeneous membrane was fabricated by a two-pot method. The illustrations were
15 shown in supporting information (Figure S2).

16 **2.2 Characterizations**

17 SEM images were taken in the field-emission mode using Hitachi S-4800. UV-visible
18 absorption spectra were recorded by UV-3600 spectrometer (Shimadzu, Japan). TEM
19 images were captured by the field-emission mode using JEM-2100f. Small-angle X-ray
20 scattering (SAXS) were used by XEUSS, Xenocs, France. AFM was used in a tapping
21 mode (MultiMode 8, Bruke).

22 **Salinity gradient energy conversion tests.** The performance of salinity gradient
23 energy conversion was tested with a Keithley 6430 semiconductor picoammeter
24 (Keithley Instruments, Cleveland, OH) using a costumed device. The tested window
25 area was $3 \times 10^{-8} \text{ m}^2$ and a pair of lamellar Ag/AgCl electrode was used. Asymmetric

1 concentrations of NaCl electrolyte were immersed into the corresponding reservoirs.
2 We simulated the sea water and river freshwater using 50-fold concentration gradient
3 (0.5 M| 0.01 M NaCl).

4 **Localized heating experiments.** The light was illumined from the one side of cell
5 (Figure 4a). The wavelength was more than 400 nm. The xenon lamp is kept a distance
6 of 5 cm from the membrane and its power was 50 W. The direction of light illumination
7 is opposite to that of concentration gradient. The temperatures of silicon wafer pairs
8 were tested by thermocouples (Type K calibration, Omega Engineering Inc.).

9 **Permeation experiments.** They were performed by a two-cell system separated by
10 membrane. The permeability rate of rhodamine 6G and sulforhodamine were tested
11 separately in order to avoid the interference. The MOF-including side was facing the
12 feed solution and it contained either 0.1 mM rhodamine 6G or sulforhodamine aqueous
13 solution. The permeability was monitored using a spectrofluorophotometer (RF-
14 5301PC, SHIMADZU, Japan).

15 **Conductance test and I - V scanning.** These two tests were tested with a Keithley
16 6430 semiconductor picoammeter (Keithley Instruments, Cleveland, OH). The tested
17 area of conductance is $3 \times 10^{-8} \text{ m}^2$ (Figure 2c, d) and that of I - V scanning is $1.26 \times 10^{-5} \text{ m}^2$
18 (Figure 2a and b).

20 3. Results and Discussion

21 As a fascinating class of porous crystalline materials, MOFs have been intensively
22 investigated due to their regular and tunable pore structures in the last decade.[15]
23 Particularly, porphyrinic MOF exhibits excellent thermal and chemical stabilities.[16]
24 Compared to 2D MOFs, the three-dimension counterparts usually aggregate in polymer
25 matrix to afford a micro-size particle, which limits their application as fillers in

1 composite membranes. Building on our early work, ultrathin zinc (II) tetrakis
2 (4carboxy-phenyl) porphyrin) (ZnTCPP) MOF nanosheets were synthesized under a
3 surfactant-assisted solvothermal method[17]. The flexible and transparent nanosheets
4 were then obtained after exfoliation under the assistant of ultrasonication with a
5 thickness of *ca.* 4~5 nm (**Figure 1a**, Figure S3). The pore size of ZnTCPP was estimated
6 at ~1.3 nm,[17] generating from the four-coordinated porphyrin units. The X-ray
7 diffraction (XRD) pattern confirmed the crystalline structure where the dominant peaks
8 centered at 7.6 and 19.4°, representing the miller indices of (002) and (004) (**Figure**
9 **1b**). With the MOF nanosheets in hand, we then prepared the ion selective membranes
10 *via* a two-step method. A sulfonated polysulfone (SPSF) solution (in *N*-methyl
11 pyrrolidone, NMP) was casted onto a clear Si wafer and dried at 85 °C for 11 hours to
12 afford a substrate. Subsequently, a mixture consisting of sulfonated polyether ketone
13 (SPEEK) and MOF nanosheets in ethanol was spin-coated onto the SPSF substrate. The
14 resultant membrane was immersed into ultrapure water until it peeled off from the wafer
15 automatically. The MOF nanosheets were uniformly dispersed in the mixture under
16 ultrasonic oscillation before spin-coating (Figure S4) and dispersed in SPEEK matrix
17 (Figure S5). The cross-section SEM image revealed the asymmetric structure of the
18 resultant membrane (**Figure 1c**). Specifically, the total thickness of the membrane was
19 4.3 μm with a SPEEK-MOF mixed matrix top layer of 300 nm (inset of Figure 1a). No
20 clear boundary was observed at the interface between the top layer and the substrate
21 due to their excellent compatibility. Of particular note, multiple spin-coating of the
22 SPEEK-MOF solution (5 times) resulted in an undesirable gutter at the interface due to
23 the mismatched surface tension (Figure S6). What' s more, because of the different
24 exchange rate of solvent and air along vertical direction in the process of solvent
25 evaporation, a denser layer was observed at the bottom of SPSF substrate. The violent

1 volatilization of solvents (i.e. ethanol) accounted for the rougher surface of top layer.
2 Thus, the AFM Ra and Rq values of SPSF were 0.688 and 0.536 nm while those of
3 SPEEK were 1.02 and 0.815 nm, respectively (**Figure 1d and e**). Because both
4 employed polymer precursors are ionomer components, a distinct phase separation can
5 be observed. For SPEEK, the dark regions represent the hydrophilic phase[18, 19],
6 while the dark regions denote the hydrophobic phase in the case of SPSF[20]. Due to
7 high degree of sulfonation, the ion clusters aggregated leading to the generation of ion
8 domains. The dark regions of SPEEK were spherical with a diameter of 11 to 13 nm
9 (Figure S7) and the ion domains of SPSF were segmentally linear. The hydrophobic
10 portion of the polymer precursor provides mechanical strength and the hydrophilic
11 phase usually forms ion clusters[19], which was further investigated by SAXS (**Figure**
12 **1f and g**). We observed double peaks for both SPEEK and SPSF. The q values of SPEEK
13 and SPSF were 0.46, 1.42 \AA^{-1} and 1.25, 2.91 \AA^{-1} , respectively. The corresponding ion
14 clusters were 13.65, 4.42 \AA and 5.02, 2.16 \AA , respectively. Furthermore, the cross-
15 section TEM image of dyed membrane sample indicated different degree of sulfonation
16 between SPSF and SPEEK (Figure S8). The color darkness increased with the
17 sulfonation degree due to the strong electrostatic interaction between sulfonated units
18 and dye molecules. The fabricated membrane possessed unprecedentedly high
19 transmittance despite of MOF incorporating (Figure S9). Notably, the composite
20 membrane possessed good mechanical strength, excellent free-standing and folding
21 features due to the compact polymeric structure. Specifically, a 4 μm -thick, 1 cm-wide
22 membrane sample could hang a weight load of 300 g up (Figure S10).
23 Thermogravimetric analysis (TGA) curves revealed a high thermostability more than
24 250 $^{\circ}\text{C}$ (Figure S11).

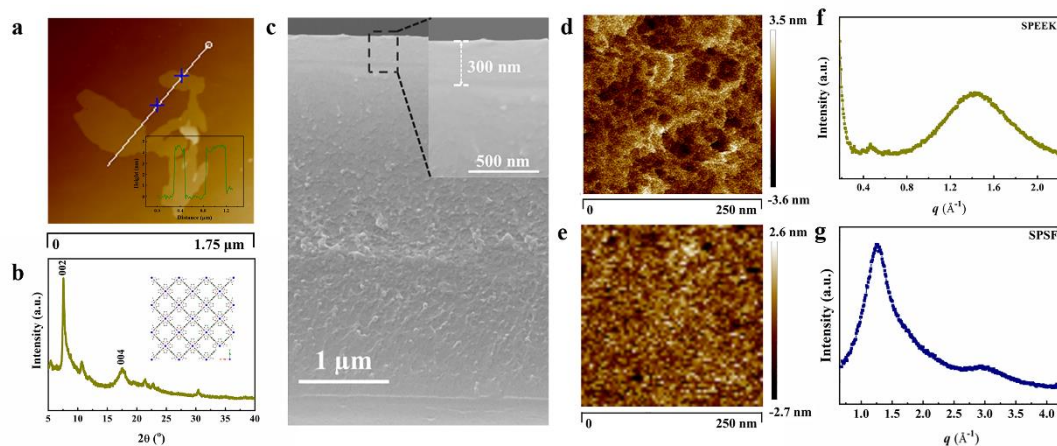
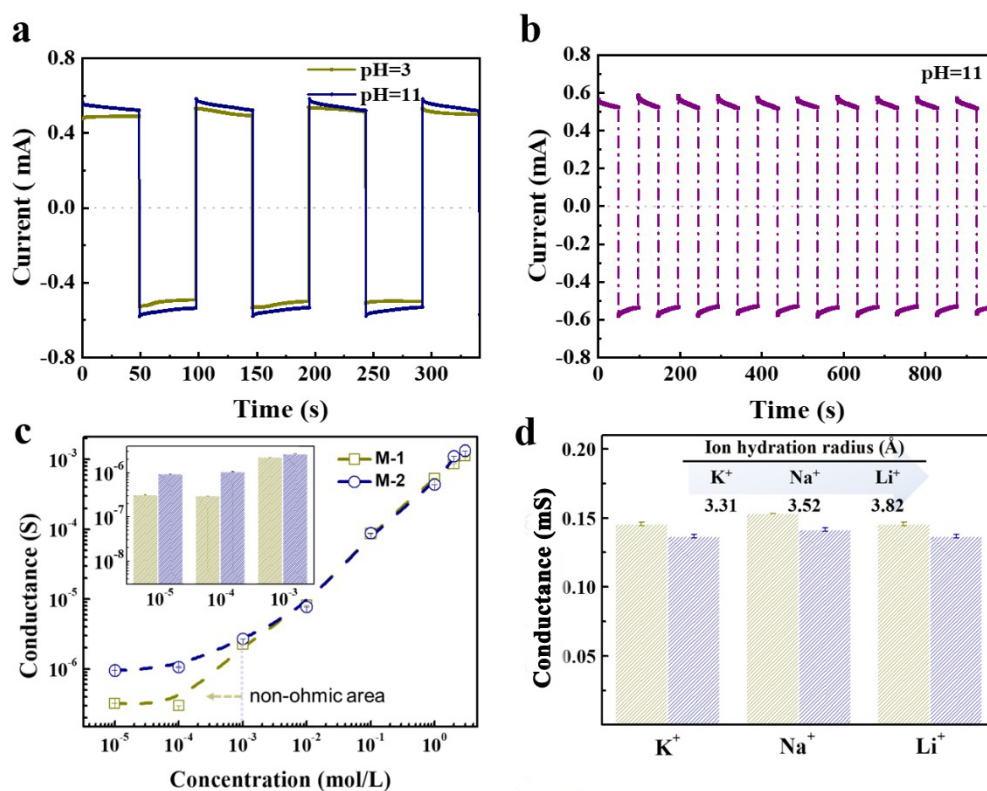


Figure 1. SPEEK-MOF/SPSF composite membrane. (a) AFM image of ZnTCPP and corresponding height profile of ZnTCPP nanosheets. (b) XRD pattern and chemical structure. (c) Cross-section view of SEM image of membrane including its border images with high resolution. (d) and (e) AFM images of pristine SPEEK layer and SPSF layer, respectively. (f) and (g) SAXS patterns of pristine SPEEK layer and SPSF layer, respectively.

We next sought to examine the ion transport performance of the MOF embedding heterogeneous membranes. The pristine SPEEK/SPSF membrane was denoted as M-1, and the MOF incorporating composite membrane was named as M-X (X=2, 3, 4, which corresponds for MOF in terms of wt.% to SPEEK 0.38, 0.73, 1.44). For M-1, no matter at which bias (negative or positive voltage), the obtained current at alkyl electrolyte was far more than that at acid electrolyte (**Figure 2a**). Its pH responsive feature is accounted for the sulfonic groups ($-\text{SO}_3\text{H}$), which is similar with biological prototype. The stability was estimated by repeated constant voltage scanning (**Figure 2b**). The performance was robust and convincing even if suffering alkali condition. The pH-responsive property and tolerance to extreme condition provide a solid benchmark to potential application. The transmembrane ionic conductance was tested in KCl solution under variable concentrations. The concentration of M-2's conductance deviated from bulk phase was higher than that of M-1. This result suggests more regions are governed by surface charge (**Figure 2c**). The linear I - V curves at ultrahigh concentration reveal a

1 suppressed concentration polarization (CP) effect due to the asymmetric structure
 2 (Figure S12).¹⁰ The conductances of different ions were estimated using 0.1 M aqueous
 3 solution. Owing to the smaller aperture of ZnTCPP, the conductance of M-2 was less
 4 than that of M-1 for Li^+ , Na^+ and K^+ ions (**Figure 2d**). The conductances indicated that
 5 the nanosheets could reduce inefficient oversized ion channel in the polymeric
 6 membrane. The ion selectivity was investigated using Rhodamine (Rh) 6G and
 7 sulforhodamine (s-Rh). They have characteristic fluorescence emission spectra and
 8 hence their permeabilities were determined by spectrofluorophotomete. The
 9 permeability of Rh was higher than that of s-Rh, which indicated that M-2 had cation
 10 selectivity due to the negatively charged sulfonic groups (Figure S13).

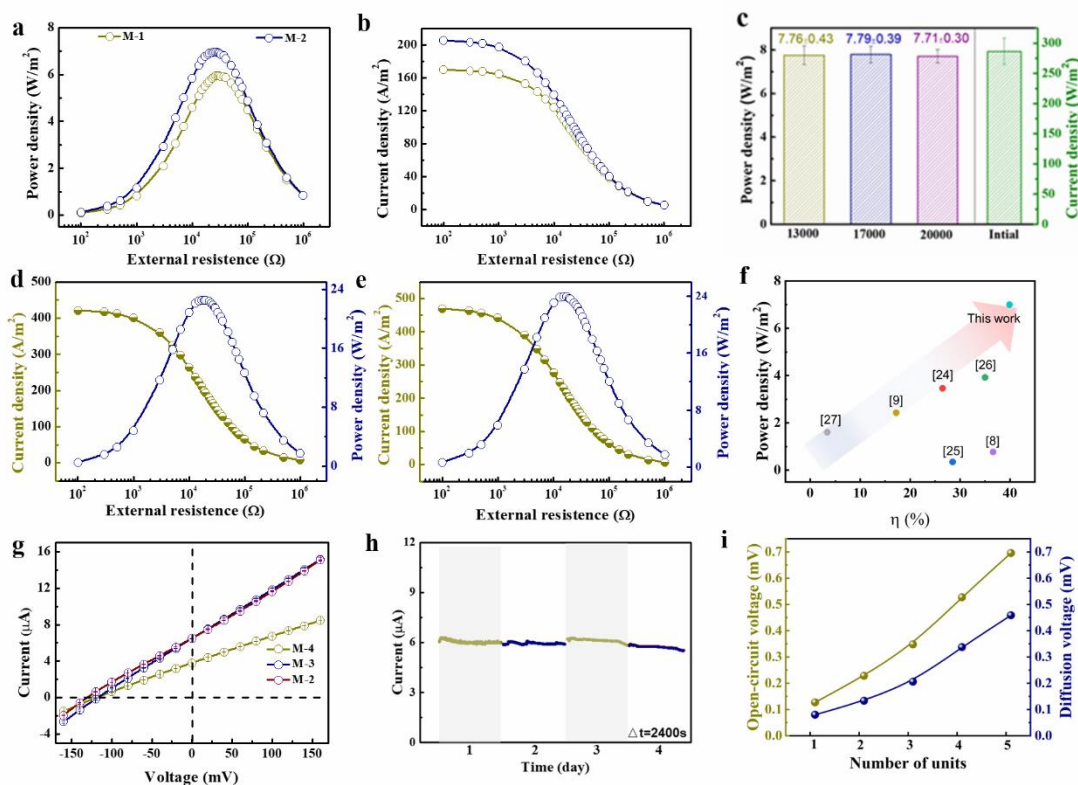


11
 12 **Figure 2.** Ion transport property of the presented composite membrane. (a) Ion current of M-1 under
 13 different pH stimuli, which means that the ion transport could be regulated by external stimuli like
 14 its biological counterpart. (b) The stability of M-1 under pH 11 regulated by voltage. (c)
 15 Transmembrane ion conductance of M-1 and M-2. The conductance of M-2 was lower than that of
 16 M-1 at high concentration while was higher at low concentration due to the tiny aperture of ZnTCPP
 17 (in the inset). (d) Conductances of M-1 and M-2 for different ions.

1
2 To benchmark the energy conversion performance, we compared the presented MOF
3 incorporating heterogeneous membrane with other, state-of-the-art flexible membranes.
4 Under 50-fold concentration gradient, the energy conversion performance and power
5 density were investigated. Conventional SPSF membranes displayed an unsatisfactory
6 performance with the open-circuit voltage, short-circuit current and power density of
7 99 mV, 2.64 μA and 2.7 W m^{-2} respectively, limiting their practical application (Figure
8 S14). In contrast, the power density and current density of the SPEEK/SPSF composite
9 membrane (M-1) increased remarkably by more than one-fold to 5.95 W m^{-2} and 170 A
10 m^{-2} , respectively (**Figure 3a, b**). The free-standing SPEEK membrane were also
11 fabricated, which was obviously weaker than SPEEK/SPSF composite (Figure S15).
12 Thus, the enhanced performance is accounted into the contemplative design of
13 heterogeneity including different sulfonation degree (charge density), pore size
14 distribution and so on. When decreasing the sulfonation degree of SPSF from 35% to
15 10% or 5%, the collected current reduced dramatically. Because too small sulfonation
16 degree place restrictions on ion flux, the difference in sulfonation degree should be
17 adopted within a proper range (Figure S16). In addition, pore generation strongly
18 depends on the exchange rate of solvent and air during solvent evaporation process. The
19 higher boiling point (bp), the faster would be the exchange rate of solvent and air. We
20 replaced the NMP (bp: 203°C) with a lower boiling point solvent *N, N*-
21 dimethylformamide (DMF, bp: 153°C) and prepared a membrane sample under the
22 same condition. The capability of such membrane was 4.78 W/m^2 , weaker than that of
23 M-1 (Figure S17). Theoretically, fast exchange rate would result in the generation of
24 larger pores. Relatively fast volatilization of DMF had a deleterious effect on the pore
25 structure.

1 Note that once introducing ZnTCPP nanosheets into SPEEK top layer, the power
2 density was enhanced to 6.96 W m^{-2} . The output power increased by about 17% in
3 contrast to pristine composite membrane (M-1). The MOF nanosheets' extremely high
4 porosities, along with direct-passing pore shapes and nanochannel in the interlayer are
5 able to maximize their 2D geometry advantages (Figure S18). The void in the hybrid
6 interfaces may generate multi-dimensional flow in the nanochannel. These advantages
7 could reduce ion transport resistance as well as suppress the geometric restriction effect,
8 meanwhile maintaining the selectivity due to their tiny aperture. The geometric
9 restriction effect often exists in SPEEK membrane, such as channel tortuosity, narrow
10 transport path and wide size distribution. As previously mentioned, the charge density
11 can be enhanced by external pH stimuli. Similar with electric-field driving force, the
12 ion acceleration can be achieved in the aspect of salinity gradient. A membrane was
13 fabricated half a year ago. We tested power densities of three external load (13000,
14 17000 and 20000 Ω) and current density of 100 Ω at the condition of pH 11 in **Figure**
15 **3c**. The maximal power density could achieve 7.9 W m^{-2} . The composite membrane
16 showed excellent acid and alkali resistant (Figure S19). In order to choose optimized
17 configuration, a 500-fold concentration gradient (5M/0.01M NaCl) was adopted
18 (**Figure 3d, e**). The power densities increased to 24 or 22.57 W m^{-2} for the cases of
19 SPEEK-MOF/SPSF or the opposite SPSF/SPEEK-MOF (to exchange the direction of
20 concentrated side), respectively. The power generation performance was attributed to
21 the designed asymmetric geometry.[21] When the MOF concentration increased, a
22 sharp decrease in energy conversion performance was observed (**Figure 3g**). The open-
23 circuit voltage and short-circuit current decreased from -130.7 to -120.5 or -118.4 mV
24 and the short-circuit current decreased from 6.5 to 6.48 or 3.79 μA , respectively (Figure
25 S20). The corresponding energy conversion efficiency (η) also decreased gradually

1 (Figure S21, Table S1). When tiny amount of fillers is added, it could distribute
2 uniformly and stack effectively, which are beneficial for improving selectivity.[22-25]
3 Thus, the decreased features can be attributed to two reasons: (1) the random stacking
4 of the excess ultrathin MOF nanosheets lead to pinhole defects and decreased ion
5 selectivity, (2) the flux of stacked nanosheets is less than polymeric membrane with
6 high sulfonation degree.[2] Optimized thickness of top layer could maximize the
7 benefit of heterogeneous structure (Figure S22). Of particular note, the transference
8 number (t_+) of M-2 reached 0.946, representing a high cationic selectivity (Table S2).
9 To emphasis the conversion capability of SGE in this study, we compared the presented
10 SPEEK-MOF/SPSF membrane with the state-of-the-art membranes reported in the
11 literature (**Figure 3f**, Table S3).[26-31] Both the energy conversion efficiency (η) and
12 the power density of the presented membrane are the highest comparing all results from
13 these literatures. Indeed, in the assessment of membrane performance many factors
14 should be considered accurately as a prerequisite of high efficiency and low-cost
15 effectiveness.[32, 33] We wish to emphasize here describing the output power with
16 $P = I \times V$ has become a practice to increase the power density. However, this is an
17 undesirable method since it represents an ideal maximal power which can't be achieved
18 in the real life. A reasonable method could be conducted under the load of external
19 resistance. In addition, a membrane-based generator was constructed to harvest SGE
20 for 96 hours (**Figure 3h**). The obtained current was stable in the long-term testing. The
21 diffusion voltage exhibited a nearly linear relationship with units of power generation
22 in series (**Figure 3i**). Each unit could generate 93 mV diffusion voltage at a
23 concentration gradient of 50.



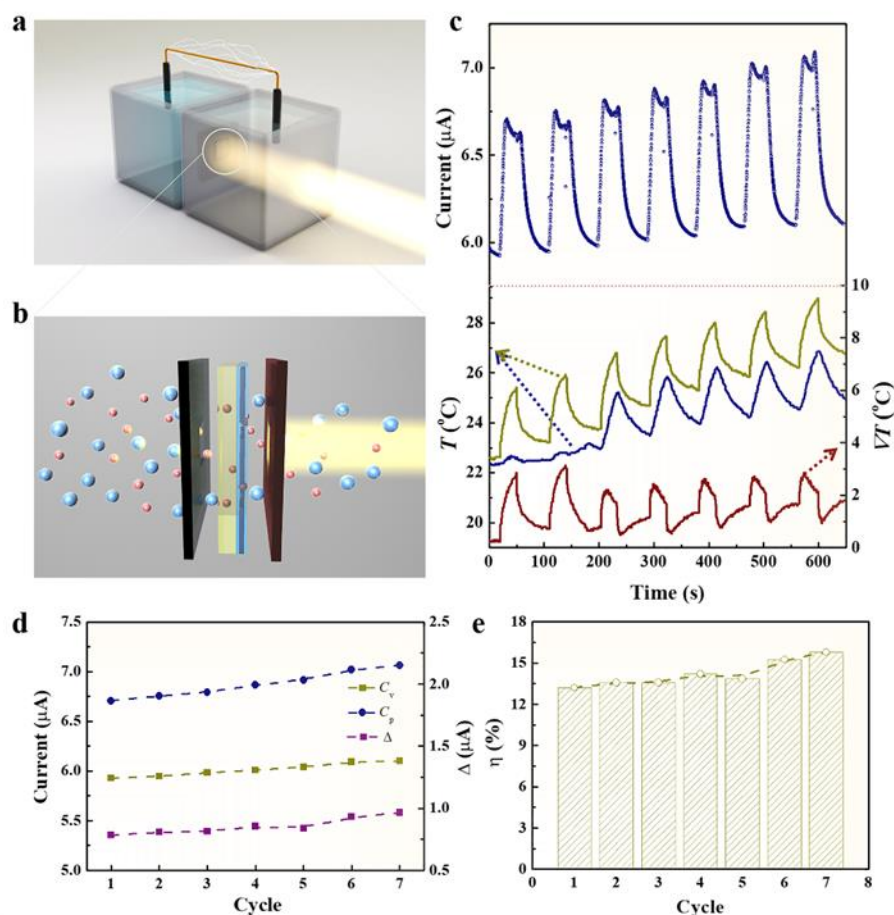
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2 **Figure 3.** Energy conversion performance. (a) The power density and (b) current density of the
 3 composite membrane with or without MOF incorporating. The MOF composite membrane
 4 exhibited an enhanced performance at a gradient of 50. (c) Power densities of three external load
 5 (13000, 17000 and 20000 Ω) and current density of 100 Ω at the condition of pH 11 and 50-fold
 6 concentration gradient. The power generation performance of (d) SPSF/SPEEK-MOF and (e)
 7 SPEEK-MOF/SPSF direction at a gradient of 500. (f) Comparison with recent advances to show the
 8 superior performance. (g) The I - V curves of different membranes under the 50-fold concentration
 9 gradient. (h) Long-term stability of the membrane-based generator. (i) The open-circuit voltage and
 10 diffusion voltage increase with the units in series.

11

12 In order to further improve power generation, we constructed a negative temperature
 13 gradient to accelerate power generation (**Figure 4a**). A pair of Si wafer was set tightly
 14 on both sides of the membrane. The localized heating was achieved by light
 15 illumination at Si wafer through the photothermal effect (**Figure 4b**, Figure S23). As
 16 shown in **Figure 4c**, the current boosted instantaneously once the light was switched
 17 “on”, which indicated an accelerated ion transport due to instant temperature gradient.
 18 The elevated current ($\Delta = 0.78\sim 0.96 \mu\text{A}$) at per circle when the light was switched “on”

1 was higher than that ($\alpha = 0.009 \sim 0.053 \mu\text{A}$) at contiguous circle when the light was
2 switched “off” (**Figure 4d**, Figure S24, Table S4). The current increased by more than
3 13% compared to pristine current without heating (**Figure 4e**). Obviously, the region
4 of both sides of the membrane was heated preferentially rather than entire bulk phase,
5 confirming that the temperature gradient worked at micro or nano scale. The elevated
6 current was accounted for the Soret effect at charged nano-confined circumstance
7 (Equation S8~10)[34] and augmented diffusion coefficients (Equation S11).[34, 35]
8 When the light was switched, the current increased in comparison with last section. It
9 was because the temperature of both sides increased. In the aqueous solution, high
10 temperature facilitated diffusive coefficients synchronously on both sides of the
11 membrane, thus promoting the ion transportation and membrane potential (Equation
12 S11). Although it has been reported the temperature of solutions played an important
13 role in rapid mass transport for highly efficient energy conversion[34] and the output
14 power could be augmented by the aid of symmetric temperature elevation,[36]
15 increasing the temperature of bulk aqueous phase is energy-intensive and challenging
16 due to extremely high specific heat capacity of aqueous solution. To overcome this
17 disadvantage, the asymmetric temperature was put forward to reduce the energy
18 consumption and boost power generation.[37] Due to the ultrafast heat transfer rate in
19 bulk phase solution, it is very difficult to generate a temperature gradient across the
20 membrane in reality. That’s why the light was adopted to subtly construct temperature
21 gradient. We are convinced that this novel design could generate temperature gradient
22 at micro or nano scale and accelerate ion transport, facilitating the power generation
23 and ion transport.



1

2 **Figure 4.** Localized heating. (a) Experiment set-up. The temperature difference was opposite with
 3 the salinity gradient. (b) Schematic illustration of the synergetic combination of salinity gradient
 4 and temperature difference. The ion diffusion rate accelerated due to negative temperature gradient.
 5 (c) Experimental results of multiple cycles. (d) The current values obtained in the “On-Off”
 6 experiment. The differences were also calculated. (e) The enhanced current percentage in the “On-
 7 Off” experiment, representing the effect of localized heating at each circle.

8

9 **4. Conclusions**

10 We have successfully fabricated a series of MOF nanosheets incorporating
 11 heterogeneous composite membranes. Benefiting from the asymmetry in chemical
 12 composition and membrane configuration, the ion transport could be boosted and
 13 regulated as required. High performance of SGE conversion attributes the success to
 14 MOF nanosheets due to their high porosity originated from long-order crystalline and
 15 nanochannel in the interlayer. In addition, taking the advantage of temperature

1 difference at small-scale region, we developed a new strategy to accelerate ion transport
2 and promote electric generation. Our work thus opens up a new avenue for the
3 development of membrane-based technology for reverse osmosis, nanofiltration,
4 electro dialysis.

5 **Declaration of competing interest**

6 The authors declare no competing financial interest.

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