

#### **Abstract**

 This research represented the first study of perfluorooctanoic acid (PFOA) decomposition using immobilized ZnO nanoparticles by electrophoretic deposition in photocatalysis and photoelectrocatalysis. Overall, considering process performance, application under visible light exposure, and cost-effectiveness, ZnO nanoparticles are highly promising for PFOA degradation. The effect of the probable production of sulfate radicals on PFOA photocatalytic decomposition over ZnO films was investigated by the addition of different concentrations of peroxymonosulfate (PMS). Notably, ~42% of PFOA was decomposed within 2 hours (rate 29 constant =  $0.287$  h<sup>-1</sup>) under UV irradiation in the presence of  $0.27$  g L<sup>-1</sup> PMS. Importantly, the same amount of PMS initiated PFOA degradation under visible light exposure with the rate 31 constant of 0.125 h<sup>-1</sup>. In photoelectrocatalysis, the optimal ZnO film demonstrated an excellent 32 degradation performance of ~49% within 2 hours at  $V = 0$  (under UV irradiation). Overall, ZnO was highly promising in both photoelectrocatalysis and PMS-assisted photocatalysis, although PMS could enhance ZnO corrosion. In addition to the sulfate radicals, the photogenerated holes and superoxide radicals were among the main active species responsible for PFOA decomposition.

 *Keywords*: Electrophoretic deposition; Perfluorooctanoic acid; Peroxymonosulfate; Photocatalysis; Photoelectrocatalysis

## 40 **1. Introduction**

41 With wide applications and environmental persistence, per- and polyfluorinated alkyl 42 substances (PFAS) have attracted extensive attention recently.<sup>1, 2</sup> Perfluorooctane sulfonic acid 43 (PFOS) and perfluorooctanoic acid (PFOA) are considered the most typical PFAS.<sup>3</sup> PFAS 44 concentration has been reported in the range of pg  $L^{-1}$  to  $\mu$ g  $L^{-1}$  in marine, ground, surface, and 45 drinking water<sup>4</sup>, while significantly higher concentration up to ~1650 mg  $L^{-1}$  has been detected 46 in some wastewater.<sup>5</sup> Notably, PFAS at concentrations of a few  $\mu$ g L<sup>-1</sup> or less accumulate in 47 organisms, and are harmful to insects, aquatic fauna, and amphibians.<sup>6</sup> Photocatalysis is 48 considered an efficient method widely used for the decomposition of various pollutnsts.<sup>7</sup> TiO<sub>2</sub> 49 is the most frequently used photocatalyst, but it has shown insignificant activity for PFOA 50 degradation, whereas In<sub>2</sub>O<sub>3</sub> and Ga<sub>2</sub>O<sub>3</sub> have yielded higher efficiencies.<sup>8-10</sup> ZnO with its lower 51 refractive index than  $TiO<sub>2</sub>$ , minimizing its light scattering and providing excellent light 52 absorption,<sup>11</sup> could be a potential alternative to TiO<sub>2</sub> for photocatalytic application. In addition 53 to its sufficient electron mobility, abundance and chemical inertness, ZnO absorbs a larger 54 fraction of sunlight than  $TiO<sub>2</sub>$ .<sup>12</sup> Considering cost-effectiveness and efficiency, the application 55 of ZnO as one of the most economical semiconductors in PFOA degradation should be 56 explored.

57 It has been suggested that SO<sub>4</sub><sup>+</sup> radicals, which take advantages of their high durability and 58 redox potential, could be generated through the activation of persulfate (PS) or 59 peroxymonosulfate (PMS) by several strategies such as UV irradiation, metal ions, heat, and 60 ultrasonication.<sup>13, 14</sup> Interestingly, PMS could be activated by heterogeneous catalysis as well, 61 where it has been effectively used to improve PFOA degradation over  $TiO<sub>2</sub><sup>15</sup>$  and  $Ga<sub>2</sub>O<sub>3</sub><sup>16</sup>$ 62 recently.

63 Photoelectrocatalysis is another prominent strategy to improve the degradation efficiency 64 of organic pollutants by accelerating the transfer of electrons from the anode to the cathode, 65 increasing the separation efficiency of electron/hole  $(e/h^+)$  pairs.<sup>17</sup> In addition, the degradation

66 capacity of pollutants could be promoted by using the bias potential in photoelectrocatalysis.<sup>18</sup> 67 The application of photoelectrocatalysis necessitates immobilization of photocatalytic materials 68 to fabricate electrodes (photoanodes). Notably, environmental photocatalysis is often criticized 69 for the inability to recover photocatalysts (in the conventional suspended form). Therefore, the 70 immobilization of photocatalysts has been a long-term challenge. There are several surface 71 engineering methods to immobilize photocatalysts, but only some of them are industrial and 72 capable of depositing solid ceramic particles. Thermal spraying and electrophoretic deposition 73 (EPD) processes are among major methods which have been widely used for the deposition of 74 different types of semiconductors. Specifically, conventional thermal spraying processes 75 including plasma, flame, and high velocity oxy-fuel (HVOF) spraying have been used to 76 immobilize  $ZnO<sub>1</sub><sup>12</sup> TiO<sub>2</sub><sup>19</sup> SnO<sub>2</sub><sup>20</sup> Fe<sub>2</sub>O<sub>3</sub><sup>21</sup> ZnFe<sub>2</sub>O<sub>4</sub><sup>22</sup> and Zn<sub>2</sub>SnO<sub>4</sub><sup>23</sup> for photocatalytic$ 77 applications. Despite of their advantages, conventional thermal spraying processes could result 78 in phase transformation of the feedstock material, due to the high heat input during spraying, 79 as observed in several cases.<sup>19, 21, 22</sup> Furthermore, the feedstock material should be suitable for 80 the specific thermal spray method. It has been suggested that the feedstock materials used in all 81 thermal spray technologies should be spherical and chemically homogeneous, with a narrow 82 particle size distribution.<sup>24</sup> The size of feedstock powders used in conventional thermal spraying 83 processes (like HVOF and plasma spray) is usually restricted in the range of 10-100  $\mu$ m.<sup>25</sup> The 84 smallest size of the feedstock powder for all spray methods is around 10 to 15  $\mu$ m.<sup>24</sup> Hence, 85 Bozorgtabar et al. used agglomerated and granulated  $TiO<sub>2</sub>$  nanopowders as the feedstock 86 material in HVOF<sup>19</sup> and air plasma spray<sup>26</sup> processes. EPD is considered another industrial 87 method of surface engineering. Based on the transfer of charged solid particles to a conductive 88 substrate under an electric field, EPD could be used for the fabrication of thick or thin 89 coatings.<sup>27</sup> EPD offers exceptional benefits including short time, simplicity, homogenous films, 90 Iow cost, and binder-free deposits.<sup>28</sup> Importantly, it is considered a non-line-of-sight process 91 and provides the possibility to coat complex shapes.<sup>29</sup> Meanwhile, simple adjustment of applied  potential and deposition time could easily control morphology and thickness of the coatings 93 fabricated by  $EDP<sup>27</sup>$  Overall, EPD could be used for deposition of various types of materials 94 including metals, ceramics, polymers, and composties.<sup>30</sup> Unlike conventional thermal spraying techniques, EPD process could take advantage of depositing nanoparticles without the need for their agglomeration. For instance, ZnO nanoparticles with different morphologies(i.e. nanorods 97 and nanosheets) have been deposited on steel sheets using EPD by Mohammadi et al.<sup>31</sup>

 Major progress has been made in the photocatalysis of PFOA in water systems, especially 99 in using TiO<sub>2</sub>, In<sub>2</sub>O<sub>3</sub>, and Ga<sub>2</sub>O<sub>3</sub>. Importantly, ZnO is much cheaper than In<sub>2</sub>O<sub>3</sub> and Ga<sub>2</sub>O<sub>3</sub>. 100 Besides, it is considered an alternative to  $TiO<sub>2</sub>$  in photocatalysis, while  $TiO<sub>2</sub>$  showed inferior 101 performance than In<sub>2</sub>O<sub>3</sub> and Ga<sub>2</sub>O<sub>3</sub> for PFOA degradation.<sup>8-10</sup> Hence, this research aimed to investigate the photocatalytic and photoelectrocatalytic degradation of PFOA over electrophoretically deposited ZnO films (fabricated by the EPD process on fluorine doped tin oxide (FTO) coated glass) to bridge the knowledge gaps in this field of research. The research findings should help to develop ZnO-based treatment process for the continuous removal of PFOA and similar recalcitrant organic pollutants in water and wastewater.

## **2. Materials and methods**

## **2.1. Materials**

 PFOA (95%), potassium peroxymonosulfate (Oxone), magnesium nitrate hexahydrate (99%), 111 FTO glass (2.2 mm thickness, 7  $\Omega$ /sq surface resistivity), sodium chloride (NaCl, >99%), sodium sulfate (Na2SO4, ≥99%), benzoquinone (BQ, ≥98%), *tert*-butanol (*t*-BuOH, ≥99.7%), disodium ethylenediaminetetraacetate (EDTA-Na2), and indium (III) oxide nano powder (In2O3, 99.998%) were purchased from Sigma-Aldrich, Australia. Zinc oxide nano powder (ZnO, 99.5%) was supplied from American Elements, USA. Ethanol was obtained from ChemSupply Australia Pty Ltd. PFOA solutions were prepared by dissolving the desired amount in Milli-Q water.

**2.2. Photoelectrochemical measurements**

 A 300-W Xenon lamp (HSX-F300, Beijing NBeT Technology Co., Ltd) equipped with a cut- off filter was used to generate visible light (~400-800 nm). Four UV lamps with the wavelength of 254 nm were employed to generate UV light. Photoelectrochemical measurements were performed using a three-electrode system (CHI-760E electrochemical workstation, CH Instrument Co., China), where ZnO electrode, Pt wire, and Ag/AgCl electrode (in saturated KCl solution) were employed as the photoanode, counter electrode, and reference electrode, respectively. Photoelectrochemical measurements included linear sweep voltammetry (LSV) and transient photocurrent (I-t curves and stability).

# **2.3. Deposition of ZnO nanoparticles by EPD**

 Commercial ZnO nanoparticles were immobilised using EPD at different deposition times (1, 2, 5, 10, and 20 min), while the voltage applied was ~30 V. It has been shown that using a two-132 step process could reduce the size and number of cracks in EPD process.<sup>32</sup> Hence, the deposition process stopped after each minute and the cathode was withdrawn from the suspension and dried in air for a couple of minutes. Before immobilization, ZnO nanoparticles (~1 g) were 135 added to ethanol  $(\sim 100 \text{ mL})$ , to which magnesium nitrate hexahydrate  $(\sim 13 \text{ mg})$  was added as the surfactant. To provide a semi-stable colloidal solution, the mixture was sonicated for 2 h. 137 In order to immobilise ZnO nanoparticles, FTO plates  $(4 \text{ cm} \times 6 \text{ cm})$  were immersed into the 138 colloidal solution where the distance between the cathode and anode (i.e. FTO plates) was  $\sim$ 1.5 cm. A TTi EX354RD dual power supply was used to provide direct current (DC). To prevent sedimentation of ZnO nanoparticles, the colloidal mixture was gently stirred using small magnetic bars during the EPD process. Finally, the fabricated ZnO films were dried in air 142 followed by the annealing treatment at 400 °C for 2 h. Notably, to study the surface topography

 and morphology, ZnO nanoparticles were immobilized on FTO plates with the size of 1.5 cm 144  $\times 1.5$  cm.

## **2.4. Photocatalytic and photoelectrocatalytic degradation of PFOA over ZnO films**

 Photocatalytic and photoelectrocatalytic experiments were conducted in 100 mL of PFOA 147 solution  $(-53 \text{ mg } L^{-1})$ . Prior to light irradiation, ZnO electrodes were immersed in the initial PFOA solution for at least 0.5 h to achieve the adsorption-desorption equilibrium. A syringe 149 was used to withdraw solution at regular time intervals; a Chromafil syringe filter  $(0.22 \mu m)$  was used to filter the solution before analysis. A liquid chromatograph-mass spectrometer (LC- MS 8060, Shimadzu) was used to analyse the concentration of PFOA and its degradation 152 products. A LC column from Phenomenex  $(2.1 \text{ mm } i.d. \times 100 \text{ mm})$ , particle size 5 µm) was used for the separation of PFOA, using Milli-Q water and methanol as mobile phases. The injection 154 volume and flow rate were 1  $\mu$ L and 0.40 mL min<sup>-1</sup>, respectively. The mass to charge  $(m/z)$  ratio of 369.0 was used as the quantitation ion for PFOA, while the *m/z* ratios of 169.1 and 219.0 were used as the confirmation ions.

#### **2.5. Characterization methods**

 Zeiss Supra 55VP scanning electron microscope (SEM) with an operating voltage of 5 kV was used to examine the surface morphology and topography of ZnO coatings. The X-ray diffraction (XRD) patterns were examined by using a Bruker D8 Discover XRD with Cu-Kα 162 radiation at room temperature ( $\lambda = 1.5406$  °A, 40 kV, 40 mA). Quantachrome instrument 163 (Autosorb iQ2) was used to measure the BET specific surface area (BET<sub>SSA</sub>) of ZnO and  $In_2O_3$ nanoparticles.

**3. Results and discussion**

# **3.1. Characterization of ZnO films**

 A ZnO electrode was fabricated by the EPD process and analysed by XRD to clarify the stability of ZnO after immobilization. XRD patterns of the ZnO film and initial ZnO nanoparticles are compared in Figure 1. As evident, the XRD patterns are thoroughly similar, thought with different intensities, and corresponding to wurtzite phase. The higher intensity of the pattern obtained for ZnO film could be related to the increased crystallinity of the wurtzite phase due 173 to the post thermal annealing treatment of the deposited film (at  $T = 400^{\circ}$ C and t = 2 h). Notably, 174 unlike  $\text{TiO}_2$ , <sup>26</sup> wurtzite ZnO could take advantage of its high thermal stability where it has been 175 stable even after plasma spraying with its considerable high temperature.<sup>12, 20</sup>



Figure 1. Comparison of the XRD patterns from ZnO film and initial ZnO nanoparticles.

 Photoelectrochemical measurements were conducted for the ZnO photoanodes fabricated 180 at different deposition times, using  $Na<sub>2</sub>SO<sub>4</sub>(0.5 M)$  as the electrolyte, and the results are shown in Figure 2(a-f). The sensitivity of the electrochemical workstation was 0.001 A/V. As shown in Figure 2(a), all photoanodes were photoactivated in the range of 0-1 V (by comparing LSV

 results under dark and UV irradiation). Photocurrent responses (I-t curves) of the ZnO electrodes are compared in Figure 2(b), where the photocurrent response decreased by increasing the deposition time which is related to the enhanced thickness of the photoanodes produced at longer deposition times. The photocurrent response was also measured in 45 min to evaluate the stability of the ZnO photoanodes. As shown in Figure 2(c), all photoanodes exhibited good stability, clarifying the good quality of ZnO films. As shown in Figure 2(d), similar to UV irradiation, the ZnO electrode was photoexcited in the range of 0-1 V under visible light irradiation (though marginally). The relevant I-t curves are compared in Figure 2(e), where the corresponding response under UV irradiation is considerably higher than that under visible light illumination which is related to the wide band gap energy of ZnO nanoparticles. The stability of the photocurrent responses under UV and visible light irradiation is compared in Figure 2(f), where a good stability was obtained under visible light irradiation as well. It should be noted that the irradiation intensity of UV source (32 W) was remarkably lower than that of visible light source (300 W). Overall, the photoanode fabricated at 1 min showed the highest photocurrent response and stability, it was therefore chosen to further assess the photocatalytic activity. The SEM surface morphology and topography of ZnO film fabricated at 1 min are shown in Figures 2(g) and 2(h), respectively.



200

202 Photocurrent response under UV irradiation (initial  $E = 0.6$  V). (c) Stability of the ZnO 203 photoanodes under UV irradiation (initial  $E = 0.6$  V). (d) Comparison of the LSV results 204 under visible and UV irradiation for the ZnO photoanode deposited in 1 min (scan rate  $= 0.1$ ) 205  $V s^{-1}$ ). (e) Comparing the photocurrent responses under visible and UV irradiation for the 206 photoanode deposited in 1 min (initial  $E = 0.6$  V). (f) Comparison of the stability of the ZnO 207 photoanode deposited in 1 min under visible and UV irradiation (initial  $E = 0.6$  V). SEM 208 surface (g) morphology and (h) topography of the ZnO film deposited in 1 min.

## **3.2. Effects of PMS and a three-electrode system on PFOA degradation**

 Before photocatalytic experiments, to activate ZnO films to achieve high efficiency, ZnO electrodes were immersed in the initial PFOA solution and irradiated by the relevant lamp (UV or visible light) for at least 3 h, followed by drying in the oven. To clarify the crucial effect of activation, two photocatalytic experiments were carried out using activated and non-activated 215 ZnO electrodes under similar conditions (PMS dosage =  $0.27$  g L<sup>-1</sup>). It should be noted that the activation process was carried out only with the presence of PFOA solution (without the addition of PMS). Notably, a fresh PFOA solution was used to evaluate the photocatalytic activity of the ZnO film after activation. As shown in Figure 3(a), non-activated ZnO film showed insignificant photocatalytic activity whereas the activated film was highly efficient. The photocatalytic activities of ZnO films with and without the addition of PMS under UV 221 irradiation are shown in Figures  $3(b)$  and  $3(c)$ .



223 Figure 3. (a) Effect of the activation of the ZnO films on PFOA ( $\sim$  53 mg L<sup>-1</sup>) decomposition 224 under UV irradiation (PMS dosage:  $\sim$ 0.27 g L<sup>-1</sup>). Plots of (b) C/C<sub>0</sub> and (c) apparent rate constant of PFOA degradation with and without the addition of PMS under UV irradiation. 226 (d) The quality of ZnO coatings before and after PMS addition. (e) Plots of  $C/C_0$  for PFOA degradation with and without the addition of PMS under visible light irradiation. (f) Photoelectrocatalytic degradation of PFOA over the ZnO film under UV illumination.

230 Three ZnO electrodes were used to clarify the photocatalytic activity of ZnO films without 231 the PMS addition. Notably, they showed different performances which could be related to their 232 different surface properties. Overall, the low efficiency of ZnO electrodes could be mainly 233 related to the significantly reduced surface area after immobilization. For screening the optimal 234 PMS dosage, another ZnO electrode was fabricated and used at different amounts of PMS (i.e. 235 0.27, 0.53, 0.80  $g L^{-1}$ ). Notably, PMS significantly improved PFOA degradation, clarifying the 236 crucial role of SO<sub>4</sub><sup>+</sup> radicals which could be considered one of the major active species 237 responsible for PFOA decomposition over ZnO. In addition, increasing PMS from 0.27  $g L^{-1}$  to 238 0.53 g  $L^{-1}$  yielded a higher performance, but further increase of PMS to 0.80 g  $L^{-1}$  caused a 239 reduction in PFOA degradation.

240 Based on the visual examination (Figure 3(d)), the quality of ZnO films showed 241 deterioration after PMS addition, which is related to the high acidity of PMS and its 242 concentration. Therefore, the ZnO electrodes were dried in the oven immediately after treating 243 with PMS to maintain their quality. Notably, the  $pK_a$  of PFOA and PMS are 0.5-3.8<sup>33</sup> and 9.4,<sup>34</sup> 244 respectively, whereas ZnO suffers from the tendency for photocorrosion especially under UV 245 irradiation.<sup>22</sup> In addition to the photocorrosion, high dosages of PMS could suppress PFOA 246 degradation due to the self-combination reaction of SO<sub>4</sub><sup>+</sup> radicals, resulting in the formation of 247 peroxydisulfates  $(S_2O_8^2)$ <sup>35</sup> which are weaker oxidants than sulfate radicals (E<sub>0</sub> = 2.1 and 2.6 248 eV, respectively).<sup>36</sup> Moreover, some other side reactions could lead to the consumption of 249 oxidant species and generation of weaker oxidants.<sup>35</sup> As a result, further increase of PMS from 250 0.53 g  $L^{-1}$  to 0.80 g  $L^{-1}$  led to the significantly reduced PFOA degradation. Considering both 251 positive and adverse effects of PMS addition, the optimal dosage of PMS was considered to be 252  $\sim$  0.27 g L<sup>-1</sup>. The corresponding apparent rate constants of PFOA decomposition were calculated 253 and shown in Figure 3(c). It should be noted that after screening, two new electrodes were used 254 to estimate experimental error (i.e. standard deviation) for the optimal dosage of PMS (0.27 g 255  $\rm L^{-1}$ ). The results of the photocatalytic decomposition of PFOA over the ZnO films under visible

 light irradiation are provided in Figure 3(e). Despite of the much higher irradiation intensity of Xenon lamp than UV lamps, ZnO coating did not show significant activity under visible light, which is mainly related to the wide band gap energy of ZnO. However, the findings were still 259 exciting from the addition of PMS (0.27 g  $L^{-1}$ ), where ~22% of the initial PFOA was degraded under visible light irradiation.

 The type of electrolyte and its concentration are among important factors affecting the 262 efficiency of pollutant decomposition in photoelectrocatalysis.<sup>37</sup> Recently, NaCl (0.05 M) was 263 used as the electrolyte for the photoelectrocatalytic degradation of PFOA over  $TiO<sub>2</sub>$  and  $TiO<sub>2</sub>$ 264 modified by graphene oxide photoanodes.<sup>38</sup> Thus, NaCl with the same concentration was used as the electrolyte in this research. Since the photocurrent response of ZnO films did not vary 266 significantly in the photoactivated range from  $0 \text{ V}$  to  $1 \text{ V}$ , as shown in Figures 2(a) and 2(d), the photoelectrocatalytic experiments were carried out under UV irradiation by applying the relative bias of 0 V vs. Ag/AgCl electrode. The results are shown in Figure 3(f), where using a three-electrode system considerably improved PFOA degradation. The enhanced PFOA removal using a three-electrode system could be contributed to the reduced recombination rate of charge carriers by transferring the photogenerated electrons to Pt electrode. In addition, 272 reactive chlorine species (RCS) including Cl' and OCl<sup>-</sup>/HOCl generated in the presence of NaCl, used as an electrolyte, could also contribute in PFOA decomposition, though mainly in 274 the final steps of PFOA degradation.<sup>38</sup> However, it seems that RCS did not play an important role in PFOA decomposition over the ZnO photoanode without using the three-electrode system (Figure 3(f)). The crucial effect of Pt electrode on improvement of the photocatalytic degradation of organic pollutants has also been reported by Su et al. which has been mainly attributed to the promoted dissociative adsorption of hydrogen and high electron affinity of Pt, 279 increasing the lifetime of photogenerated chare carriers.<sup>39</sup> The photocurrent response of all three 280 ZnO electrodes during the photoelectrocatalytic experiments at  $V = 0$  (electrolyte: 0.05 M NaCl), i.e. Figure 3(f), is shown in Figure 4 to clarify the stability of ZnO photoanodes during  PFOA degradation. As evident, all electrodes showed good stability during the whole process (2 h). It is obvious that their photocurrent response decreased gradually by PFOA decomposition. It should be noted that the plunge of photocurrent at around 2400, 4800, and 7200 s is related to turning off the UV lamps at the corresponding intervals to withdraw PFOA solution for analysis by LC-MS.



Figure 4. Stability of the ZnO electrodes during the photoelectrocatalytic experiments.





 Figure 5. Visual appearance of the ZnO electrode after (a) activation, (b) first cycle, (c) second cycle, and (d) third cycle. (e) Cyclic performance of the ZnO electrode in the presence 311 of PMS  $(\sim 0.27 \text{ g L}^{-1})$  under UV irradiation.

 The effect of PMS on PFOA degradation in the absence of ZnO was also investigated under both UV and visible light irradiation (Figure S1(a)). The vessels used for evaluation of the photocatalytic/photoelectrocatalytic decomposition of PFOA over ZnO are shown in Figure S1(b). Notably, a quartz reaction vessel with a holder was used for the ZnO electrodes, where they relied on the holder during the photocatalytic experiments; and the light source (UV or visible) was irradiated from the front side of the ZnO electrodes(Figure S1(b, i)). Since powders could become stuck in the holder, a simple vessel was used for evaluation of the photocatalytic activity of suspended ZnO nanoparticles (Figure S1(b, ii)). A wider vessel was used to evaluate the effect of PMS in the absence of ZnO (Figure S1(b, iii)). It reduces the depth of PFOA 322 solution since the initial volume was  $\sim$ 100 mL in all cases. As shown in Figure S1(a), neither UV nor visible light were able to highly degrade PFOA in the absence of ZnO (even by increasing the irradiation time). Hence, PMS alone (in the absence of ZnO as photocatalyst) did not play an important role in PFOA degradation. Similarly, as reported by Xu et al., only 18% 326 of PFOA was decomposed under UV irradiation (254 nm) within 3 h when using only PMS.<sup>16</sup> Another ZnO electrode was fabricated to evaluate the effect of irradiation time on the 328 photocatalytic decomposition of PFOA under UV irradiation with the addition of PMS (~0.27  $\,$  g L<sup>-1</sup>). As shown in Figure S2, the decomposition efficiency reached ~64% after 4.5 h while it was ~42% after 2 h (Figure 3(b)). It has been reported that the total degradation of PFOA could be achieved in PMS-assisted photocatalysis. For instance, PFOA was completely degraded 332 within 2 h when using the molar ratio of 1:1 between  $Ga_2O_3$  and PMS, while only ~58% of 933 PFOA was degraded in 3 h by using only  $Ga_2O_3$  powder.<sup>16</sup> Considering these findings, it is estimated that the total decomposition of PFOA over the ZnO film needs a prolonged time. It should be also noted that the specific surface area of the catalyst reduces after deposition on a substrate which is one of the major drawbacks of immobilization.

 The photocatalytic and photoelectrocatalytic activities of several semiconductors used for PFOA decomposition are compared in Table 1, where photoelectrocatalysis is more efficient 339 than custom photocatalysis in all cases. Notably, PFOA concentration in the range of  $\sim 50$  mg 340  $L^{-1}$  is usually higher than that detected in the polluted water,<sup>15</sup> but the initial PFOA 341 concentration in the range of mg  $L^{-1}$  has been used by other researchers (Table 1) which could 342 be related to the usually higher efficiency of degradation at higher initial concentrations. 343 However, it should be noted that the effect of the initial PFOA concentration on its degradation 344 highly depends on the type of catalyst. For instance, increasing the initial concentration from 345 20 mg L<sup>-1</sup> to 40 mg L<sup>-1</sup> and 60 mg L<sup>-1</sup> improved the rate constant of PFOA decomposition using 346 Pt-, Ag-, and Pd-modified  $TiO<sub>2</sub>$  whereas the same order of increase in the initial concentration 347 showed a reduction in the degradation rate constant using pure  $TiO<sub>2</sub>$ .<sup>40</sup>

<b>Catalyst/Electrode</b>	<b>Light source</b>	$[PPOA]_0$	<b>Photocatalysis</b>	Photoelectrocatalysis		<b>Reference</b>
		$(mg L^{-1})$		<b>Efficiency</b>	Electrolyte	
TiO <sub>2</sub> powder	Xenon lamp (300 W, 400-770 nm)	50	$0.028 h^{-1}$ (~20% in 8 h)	$\overline{\phantom{a}}$		15
TiO <sub>2</sub> power	UV (254 nm)	41.4	$0.045$ h <sup>-1</sup> (~16% in 4 h)	$\overline{\phantom{a}}$	$\qquad \qquad -$	8
In <sub>2</sub> O <sub>3</sub> powder	UV (254 nm)	41.4	$0.378$ h <sup>-1</sup> (~80% in 4 h)	$\overline{\phantom{a}}$	$\overline{\phantom{a}}$	8
$In2O3$ microspheres	UV (254 nm)	30	$~100\%$ in 20 min	$\overline{a}$		41
$In2O3$ nanoplates	UV(254 nm)	30	$\sim$ 100% in 40 min	$\overline{\phantom{a}}$	$\overline{\phantom{a}}$	41
$In2O3$ nanocubes	UV(254 nm)	30	$\sim$ 100% in 2 h	$\overline{\phantom{a}}$		41
ZnO powder	UV (32 W, 254 nm)	53	$\overline{0.090}$ h <sup>-1</sup> (~19% in 2 h)	$\overline{\phantom{a}}$	$\blacksquare$	This work
$TiO2$ electrode	$100 \text{ mW/cm}^2$	9.9	$0.006 h^{-1}$ (~2% in 2 h)	$0.03 h^{-1}$ (~5% in 2 h)	Na <sub>2</sub> SO <sub>4</sub> (0.1 M)	42
$TiO2$ electrode	UV (16 W, 254 nm)	5	$\overline{\phantom{a}}$	$0.378 \text{ h}^{-1}$ (~46% in 2 h)	NaCl (0.05 M)	38
TiO <sub>2</sub> /GO electrode	UV (16 W, 254 nm)	5	$\overline{0}$	$0.372 h^{-1}$ (~43% in 2 h)	NaCl (0.05 M)	38
$TiO2$ electrode	Low pressure Hg lamp (100 W)	40	$~14\%$ in 2 h	$-44\%$ in 2 h	H <sub>2</sub> SO <sub>4</sub> (0.1 M)	43
ZnO electrode	UV (32 W, 254 nm)	53	$0-27%$	0.331 h <sup>-1</sup> ( $\sim$ 49% in 2 h)	NaCl (0.05 M)	This work

348 Table 1. Comparison between photocatalytic and photoelectrocatalytic activity of PFOA degradation over different semiconductors.

349 Note: GO (graphene oxide)

## **3.3. PFOA photodegradation mechanism**

 The crucial role of sulfate radicals on PFOA decomposition over ZnO films was clarified in the previous section by PMS adding. To elucidate other active species, three reagents including t-353 BuOH, BQ, and EDTA-Na<sub>2</sub> were added to the initial PFOA solution to scavenge 'OH,  $O_2$ ', and 354 the photogenerated holes (h<sup>+</sup>), respectively. For simplicity, suspended ZnO nanoparticles (0.53  $\text{g } L^{-1}$ ) were used for the analysis of the active species and intermediates. As shown in Figure S3(a), the photocatalytic activity of ZnO nanoparticles was quenched considerably by the 357 addition of EDTA-Na<sub>2</sub> and BQ, clarifying the crucial role of  $h^+$  and  $O_2$ <sup>\*</sup> in PFOA decomposition, whereas the addition of t-BuOH (even at high concentrations up to 0.1 and 0.2 M) did not reduce PFOA decomposition. Notably, using high concentrations of t-BuOH could increase PFOA degradation because of its less polarity than water, leading to the higher 361 reactivity of superoxide radicals.<sup>44</sup> The intermediates formed during the photocatalytic degradation of PFOA could include PFHpA, PFHxA, PFPeA, PFBA, PFPrA, and TFA (in PMS-assisted photocatalysis using ZnO), but the shorter chains of PFOA (especially the last ones including PFBA, PFPrA, and TFA) could be hardly detected (due to their low 365 concentration) as reported by Xu et al., where  $TiO<sub>2</sub>$  was used as the photocatalyst.<sup>15</sup> The time dependence of the first three shorter chains of PFOA is shown in Figure S3(b), where PFHpA, PFHxA, and PFPeA could be respectively considered the first, second, and third generated intermediates. Overall, it is estimated that the photodecomposition of PFOA over ZnO could follow a stepwise manner from PFOA to its shorter chains including PFHpA, PFHxA, and PFPeA. The stepwise manner of PFOA degradation has been reported in several cases using 371 various photocatalysts.<sup>15, 16, 36</sup>

 The adsorption of the organic pollutant on the catalyst surface is of high importance in photocatalysis. Thus, the adsorption capacity of PFOA over ZnO nanoparticles was measured 374 and compared to that of  $In_2O_3$  nanoparticles (for control). To measure PFOA adsorption, the 375 catalysts were stirred in PFOA solution  $({\sim}53 \text{ mg L}^{-1})$  for 1.5 h in the dark. To clearly

 discriminate the adsorption capacity of PFOA over catalysts, the catalysts dosage was considered approximately 4 times higher than that used in the photocatalytic experiments (i.e. 378 0.53 g L<sup>-1</sup> as mentioned previously). The adsorption capacity of PFOA over In<sub>2</sub>O<sub>3</sub> nanoparticles was around 1.6 times higher than that over ZnO nanoparticles (~39.6% vs. ~24.8%), whereas 380 the BET<sub>SSA</sub> of ZnO nanoparticles was around 4.3 times higher than that of  $In_2O_3$  nanoparticles 381 (~30 m<sup>2</sup> g<sup>-1</sup> vs. ~7 m<sup>2</sup> g<sup>-1</sup>). For control, the photocatalytic activity of suspended In<sub>2</sub>O<sub>3</sub> nanoparticles for PFOA degradation was also investigated under UV irradiation (Figure S4). 383 Considering Figure S3(a), it is concluded that ZnO nanoparticles were more promising  $\left(\sim 21\right)$ % 384 degradation within 2 h) than  $In_2O_3$  nanoparticles (~14% degradation within 4 h). Hence, it seems that the lower adsorption capacity of PFOA over ZnO nanoparticles did not play an important role in the promising performance of ZnO for PFOA degradation.

## **4. Conclusions**

 The potential degradation of PFOA (as one of the most persistent organic pollutants) has been examined using immobilized ZnO nanoparticles (as one of the most economical semiconductors) in photocatalysis and photoelectrocatalysis modes. The probable production of sulfate radicals by the addition of PMS significantly improved PFOA decomposition over 393 ZnO films, where the high apparent rate constants of 0.287  $h^{-1}$  and 0.125  $h^{-1}$  were achieved by 394 the addition of PMS  $(0.27 \text{ g L}^{-1})$  under UV and visible light irradiation, respectively. Overall, considering cost-effectiveness, degradation efficiency, and the potential of use under visible light, ZnO films are very promising as the candidate photocatalyst for PFOA decomposition. In addition to the strong effect of PMS, ZnO electrodes produced by EPD offered high 398 efficiency using the three-electrode system (rate constant  $= 0.331 \text{ h}^{-1}$ ). Hence, ZnO films have demonstrated high capability for PFOA decomposition in both photocatalysis and photoelectrocatalysis under UV irradiation. Further research is required to develop more efficient visible light-activated photoanodes with improved photocorrosion resistance.

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